

Stay-In-Place Formwork

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Formwork in Construction



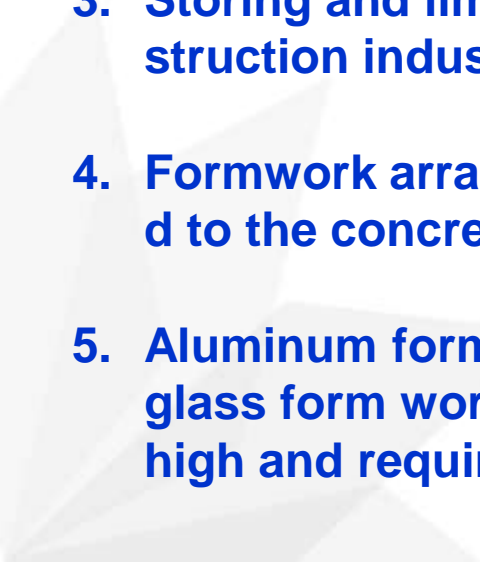


Importance of Formwork



Limitations



- 1. Wood, steel sheets/plates, ply boards, Aluminum, Plastics etc... are commonly used form work materials.**
 - 2. Formwork costs around 40-50% of the total construction cost in RCC.**
 - 3. Storing and limitations in reusing increases the capital investment in construction industry.**
 - 4. Formwork arrangement and its alignment consumes more time compared to the concreting work.**
 - 5. Aluminum form work, steel form work, vinyl based form work, rubber and glass form works are also available. But still the capital investments are high and requires maintenance, transportation, storing unit etc..**
- 

NEED OF STAY-IN-PLACE FORM WORK



Stay in place (SIP) form work system is an effective and advanced way of formwork system.

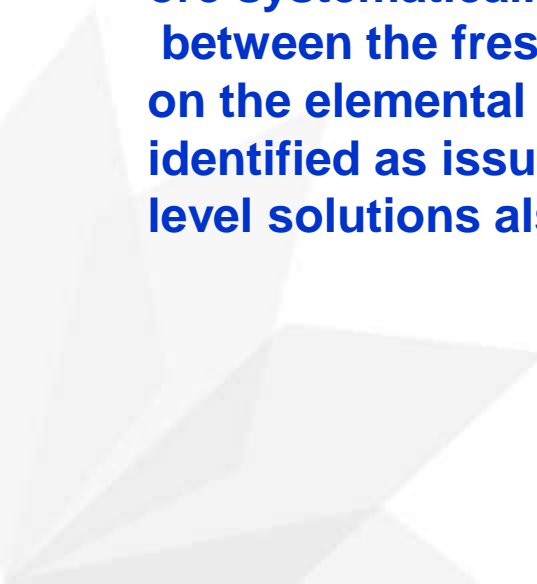
In SIP the formwork material become an integral part of the structural elements Advantages such as thermal comfort, external protection to resist the durability issues, additional confining pressure and reduces the construction time and offers viable economical solution.

Different materials such as fibers reinforced polymers (FRP), polyvinyl (PVC), Cementitious composites, extended polystyrene (EPS), glass fiber reinforced concrete/composites (GFRP), steel composites, steel meshes etc... have been in practice.



Research Scope in SIP

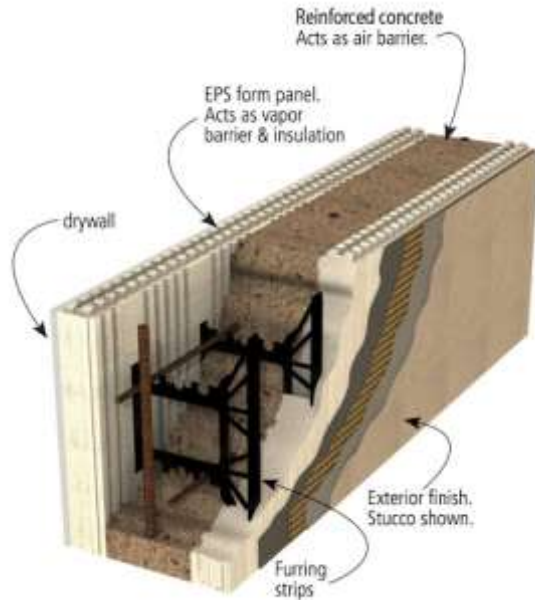
Numerous researches have focused on improving the SIP system more systematically and efficiently. Problems such as the bond between the fresh concrete and the form work materials influence on the elemental behavior, failure pattern, life span etc... have been identified as issues in SIP systems and research level and practical level solutions also had been proposed.



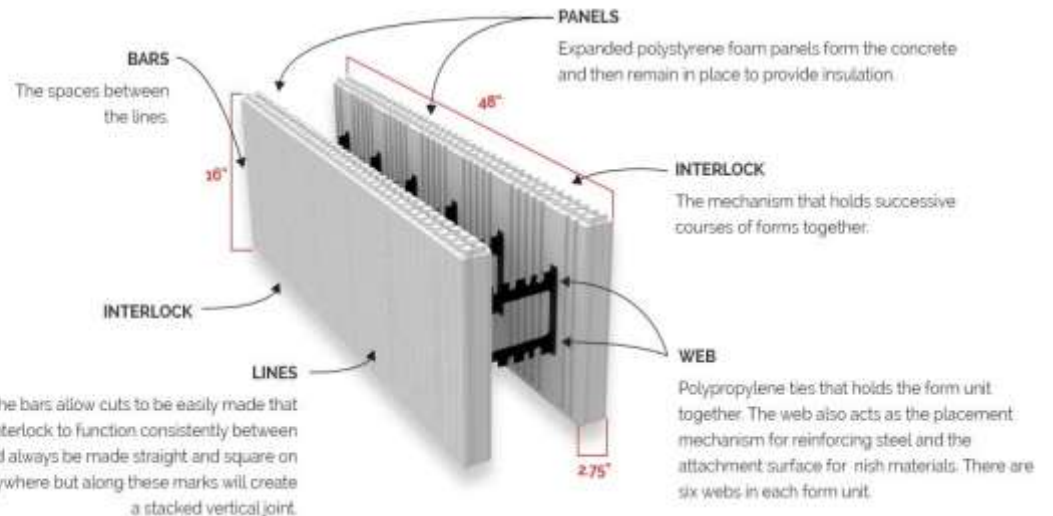
INSULATED CONCRETE FORMS (ICF)

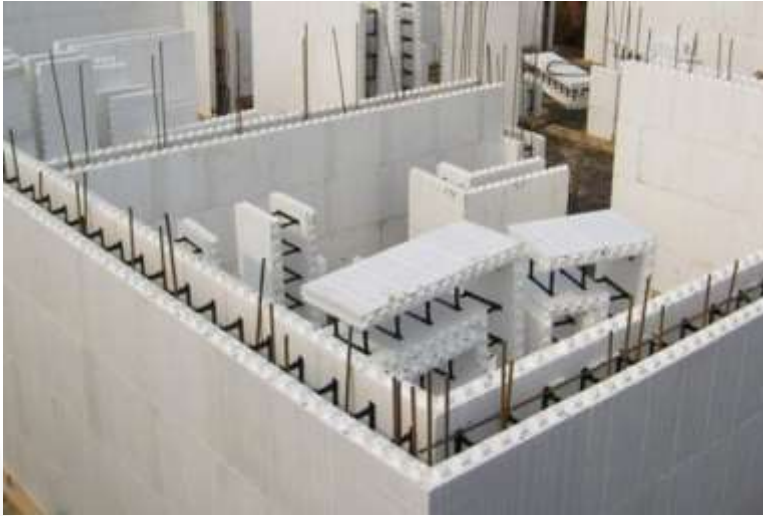


About ICFs



TYPICAL ICF FORM UNIT TYPICAL ICF WALL ASSEMBLY





Advantages

- Offers resistance to gravity and lateral loading due to its monolithic construction technique.
- Energy efficiency and thermal comfort
- Noise reduction
- Resistant to corrosion.
- Easy to install and time saving construction technique.
- Cost effective solution.

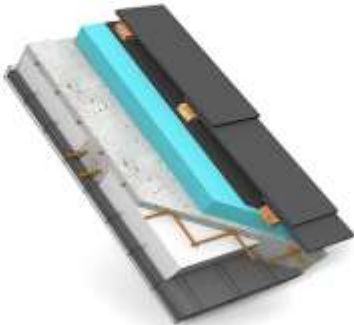
LATTICE BASED ICF SYSTEM AND ITS DIFFERENT MODULES



BEARING WALLS
Lattice + infill material + concrete
With or without reinforcement.



ROOFS
Lattice + infill panel + SISMO interjoist +
concrete + additional insulation



NON-BEARING WALLS
Lattice + infill material
With or without structural filler.

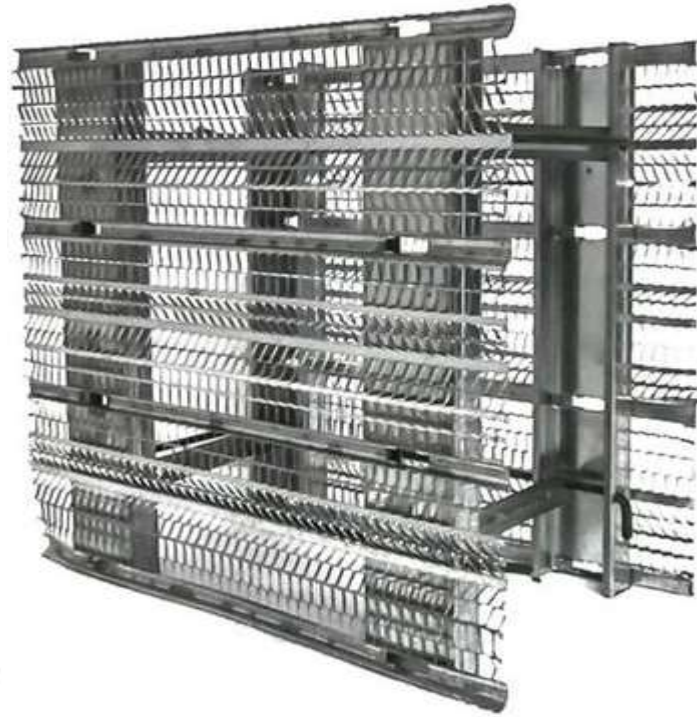


FOUNDATIONS & CELLARS
Lattice + infill material + tanking

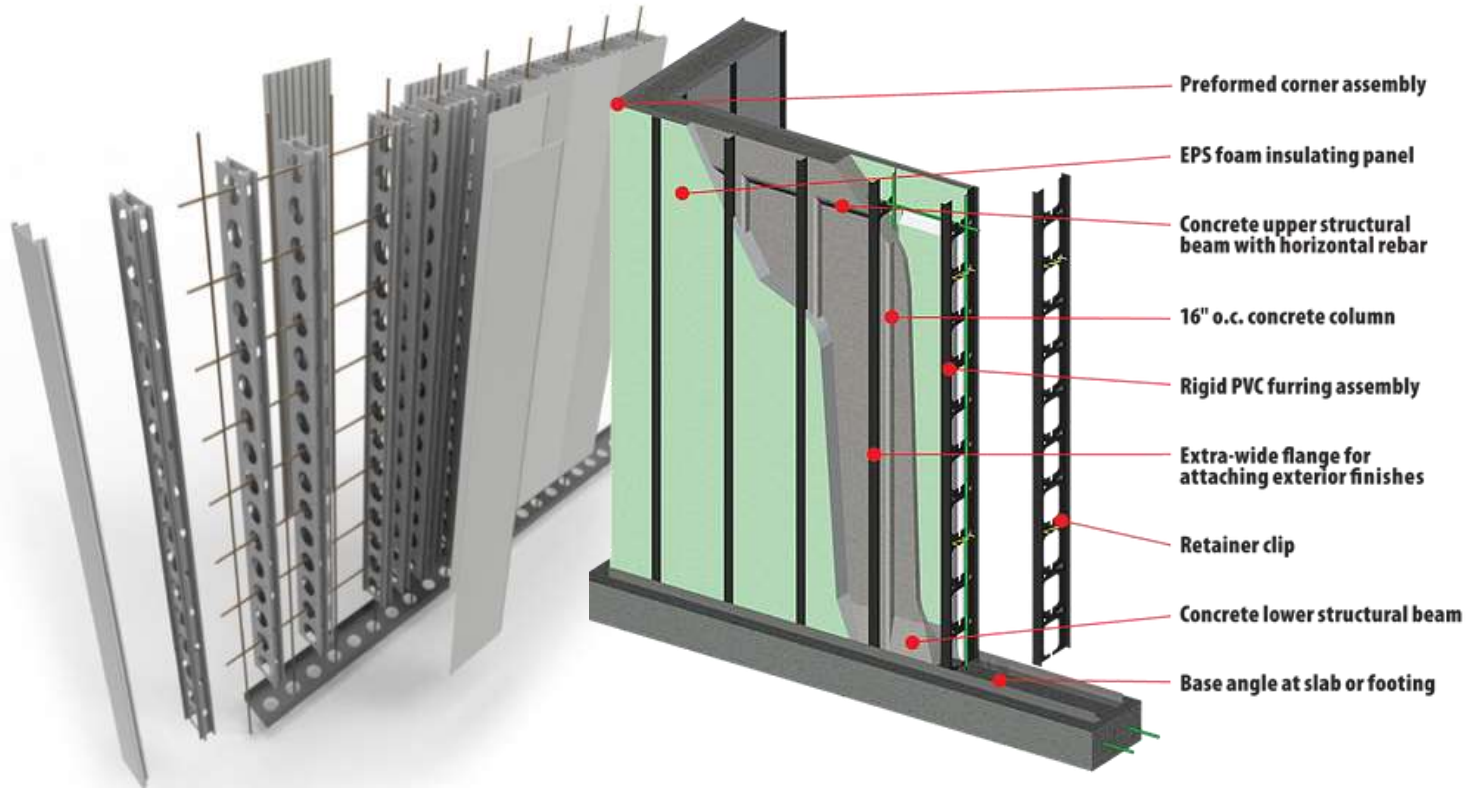


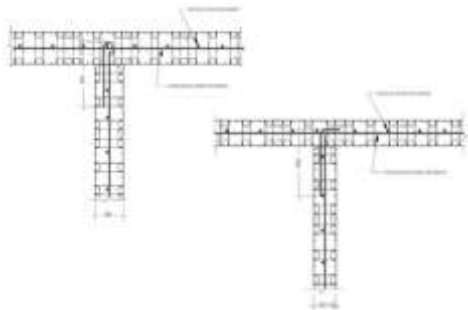
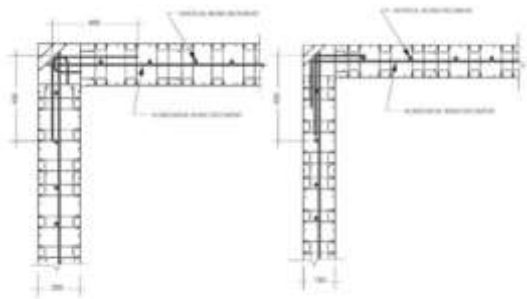
FLOOR SLABS
Lattice + infill panel +
SISMO interjoist + concrete

Structural SIP system

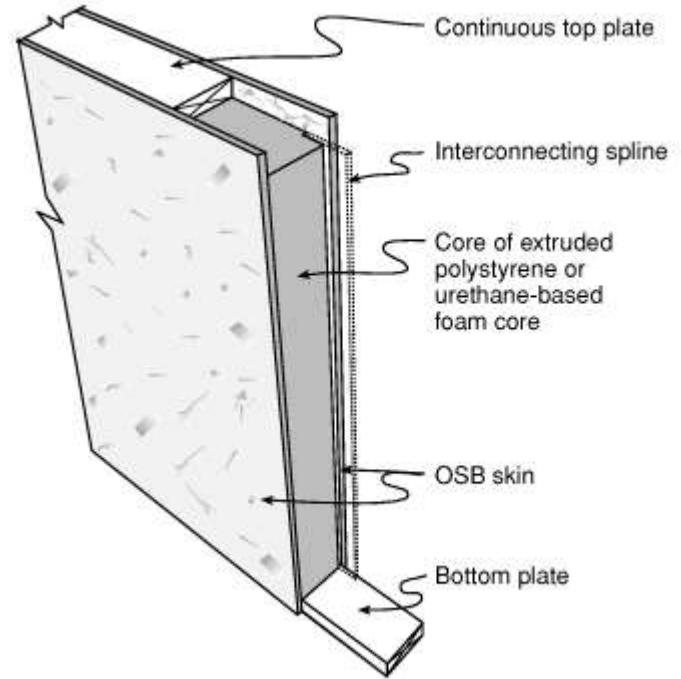
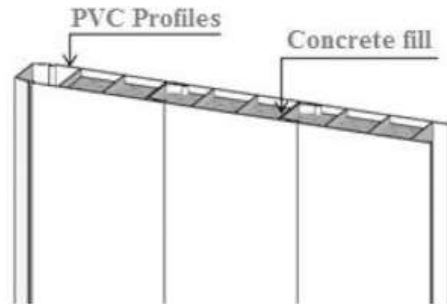
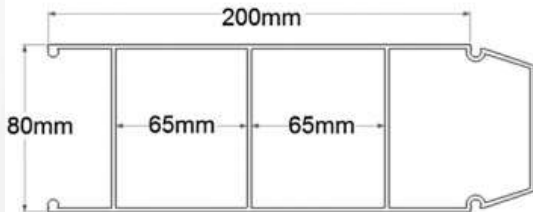
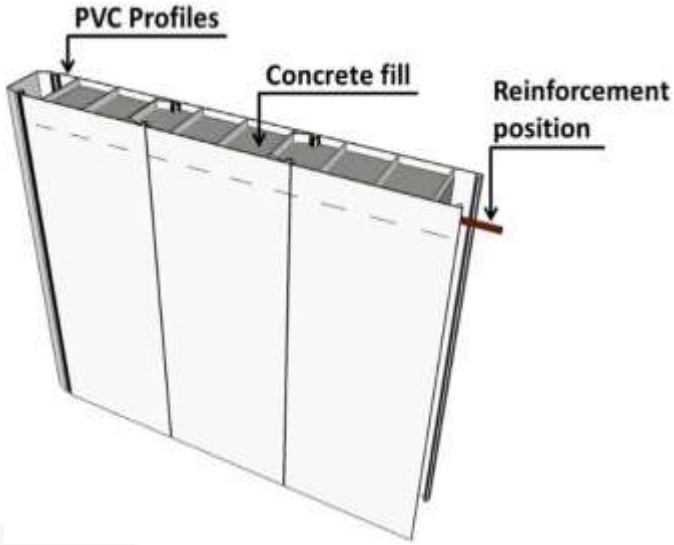


PVC Based SIP system

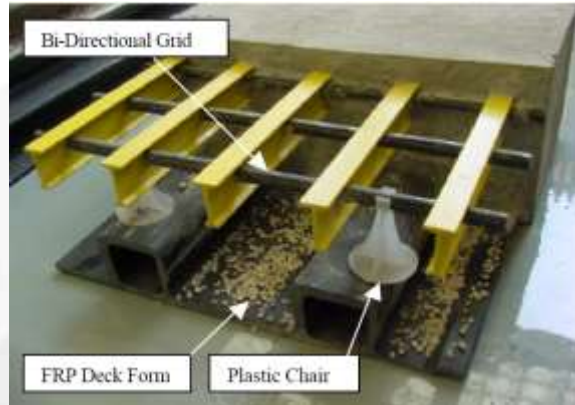
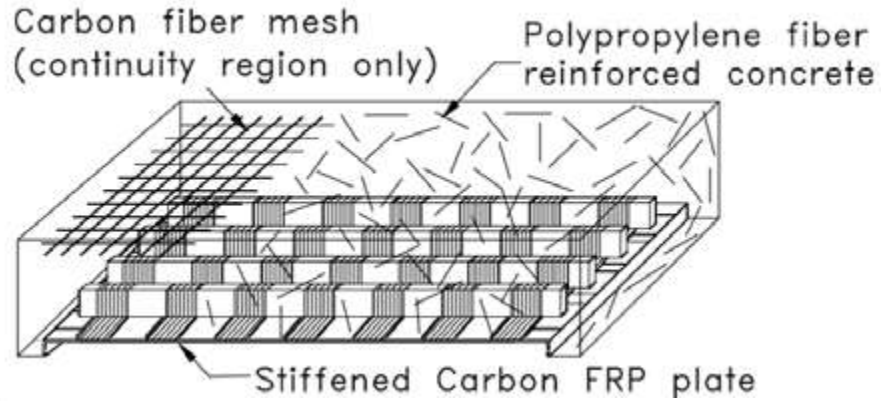


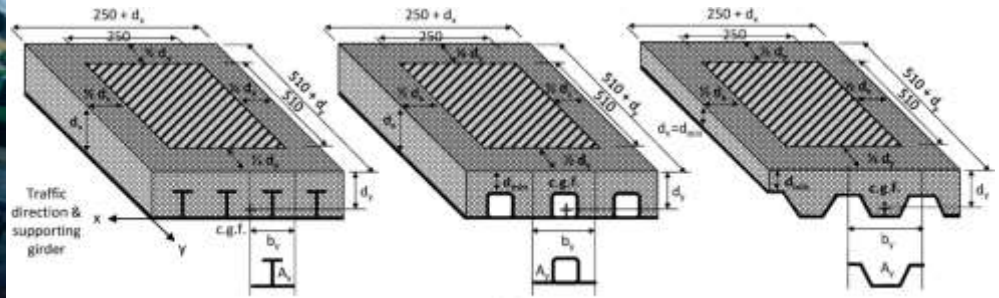


PVC Profile – Concrete Filler - SIP system

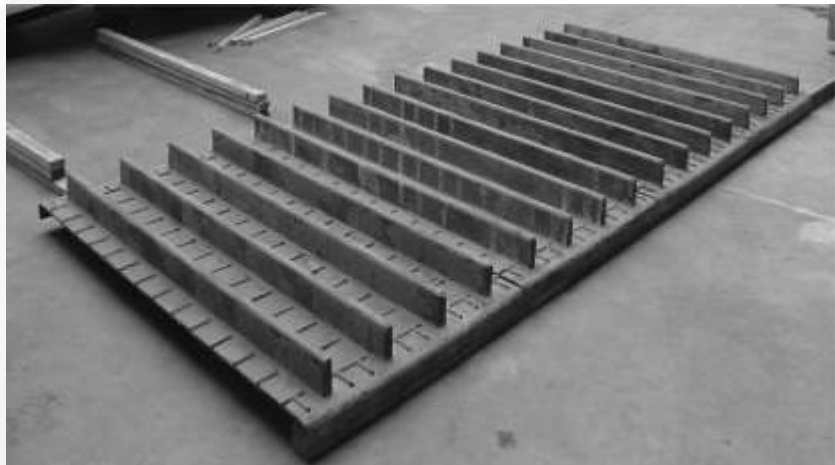


FRP BASED SIP FORM WORK SYSTEM



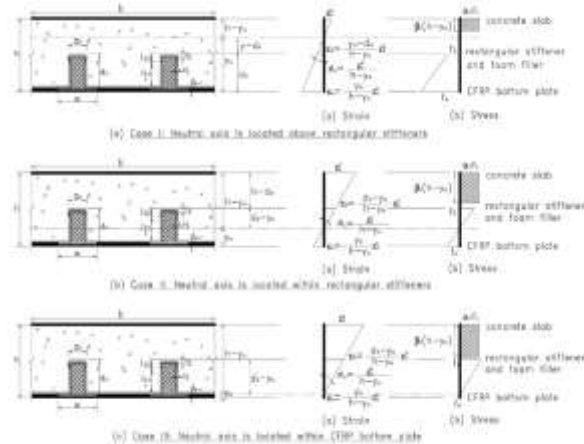
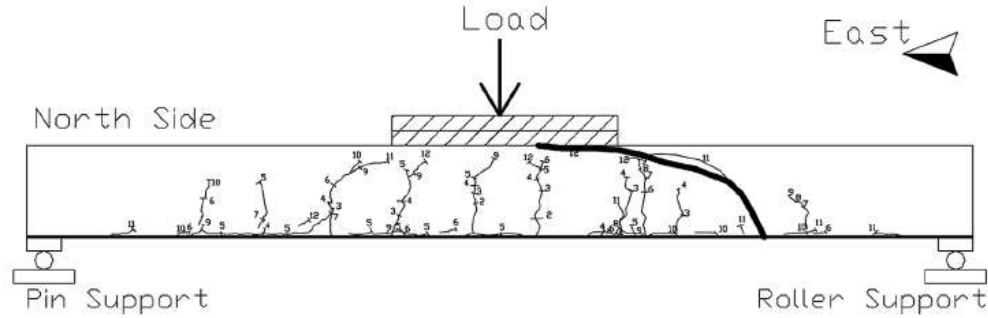


(a)

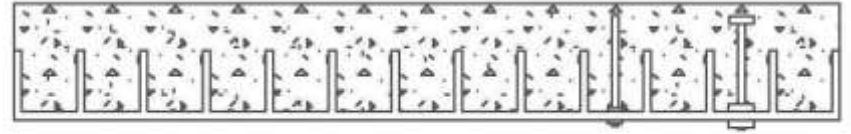


(b)

Structural Behavior of FRP SIP



FRP panel with Sand blast coating

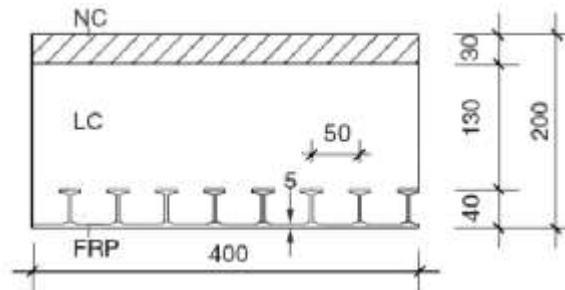
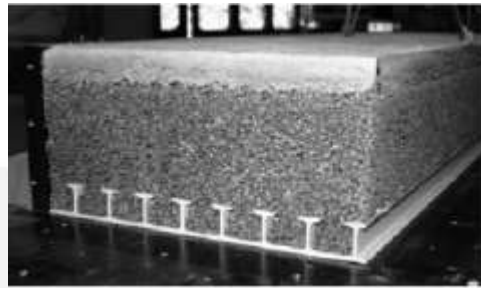


Placing of FRP Planks between the girders

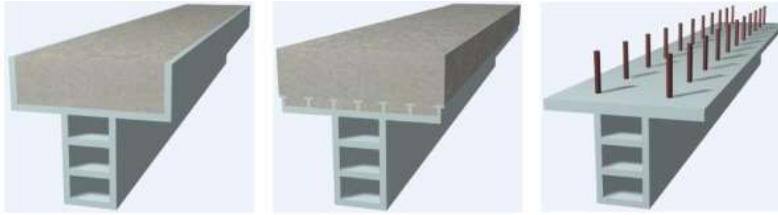


HYBRID FRP PANELS

In Hybrid FRP panels light weight concrete/foam based concrete used as core material over a thin layer of normal concrete will be used. Figure shows the Hybrid FRP panels. The bottom most FRP planks are offering better resistance to tension and the top most concrete layer offers resistance to compression. The inner core resists the shear force and acts as insulated materials. This principle increases the stiffness and strength without increasing the density of the elements.



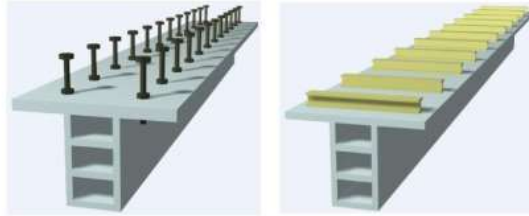
FRP Box Beam with Concrete in the Compression Zone



(a) Adhesive

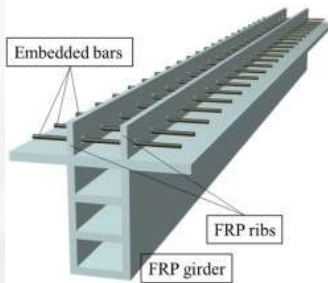
(b) Interlock

(c) FRP drawls

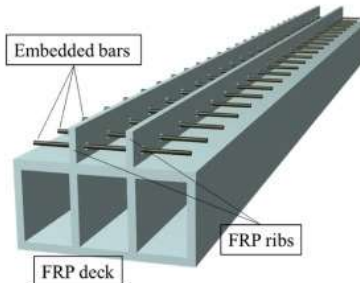


(d) Steel bolts

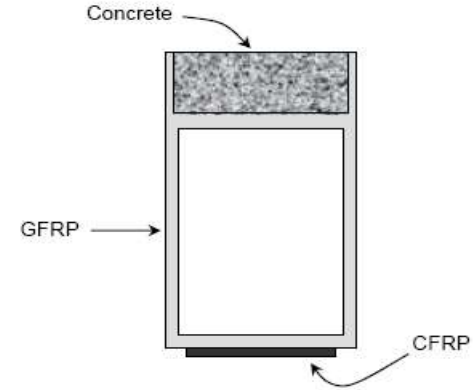
(e) FRP shear key



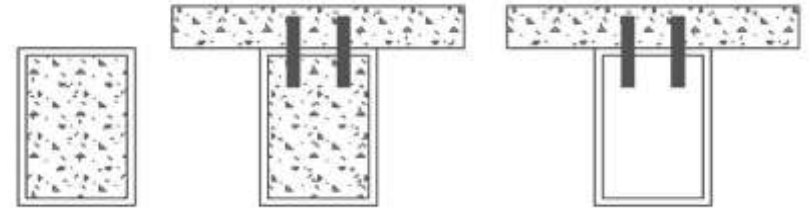
(f) PFR for hybrid beam



(g) PFR for hybrid deck



GFRP-concrete hybrid flexural member (Deskovic *et al.* 1995)



Concrete-filled FRP tubes with a concrete slab on top (Fam and Skutezky, 2006)



FRP/steel laminate

(a)

Shear studs



200mm diaphragm

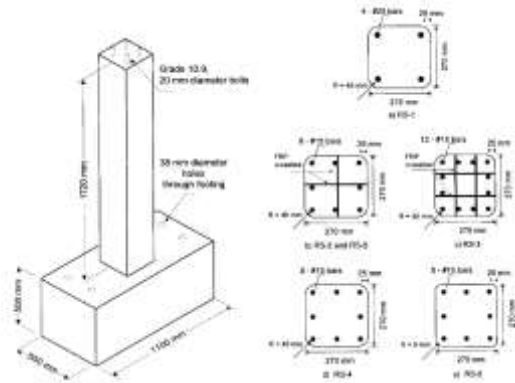
Coarse aggregate

(b)

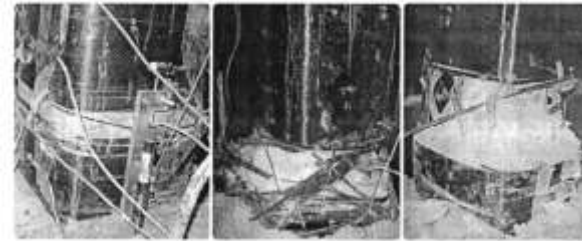


(c)

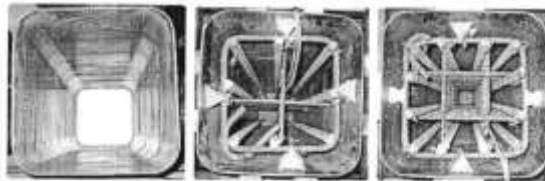
Structural Behavior of Column Constructed using FRP SIP Formwork



(a) Column RS-1 (b) Column RS-2 (c) Column RS-3



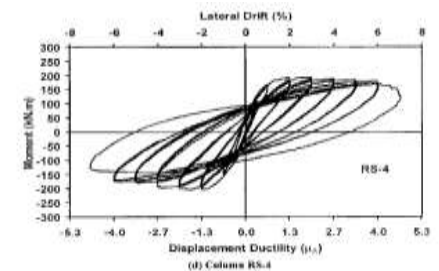
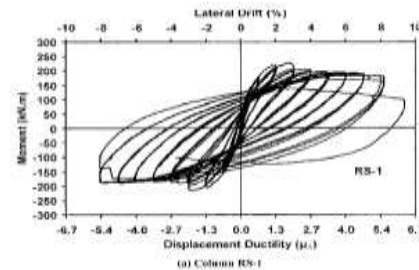
(d) Column RS-4 (e) Column RS-5 (f) Column RS-6



a) RS-1 (b) RS-2 and RS-5 (c) RS-3

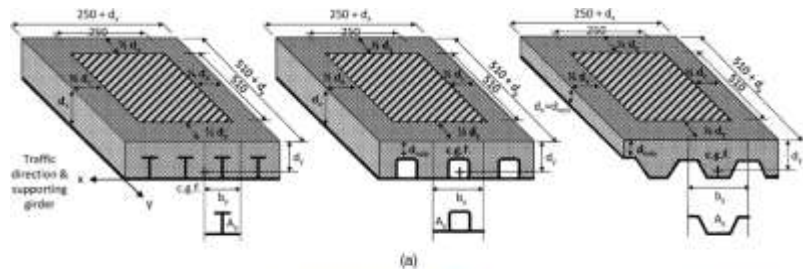


d) RS-4 (e) RS-6



Design Equations for Concrete Bridge Decks with FRP Stay-in-Place Structural Forms

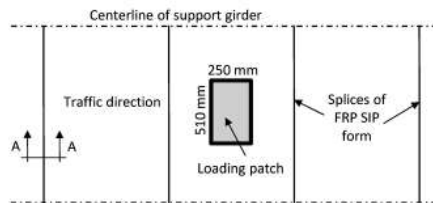
Martin Noel¹ and Amir Fam, M.ASCE²



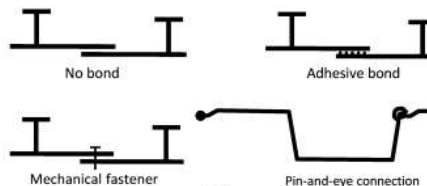
(a)



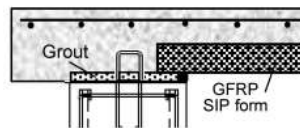
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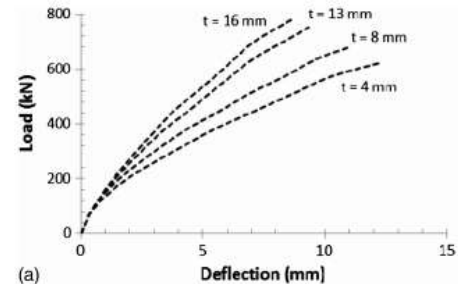
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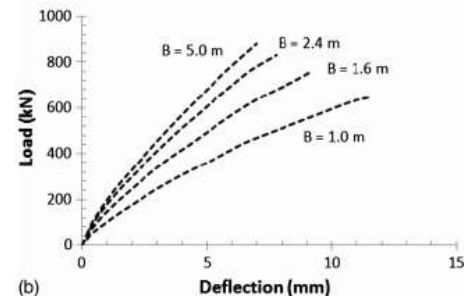
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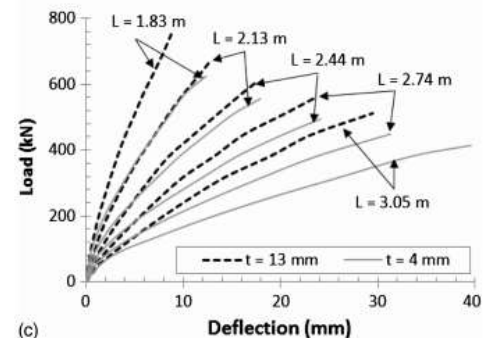
(c)



(a)



(b)



(c)

Common Detailing used in FRP SIP System



→ **T-up Stiffeners on Plate**



→ **Tubular Sections on Plate**



→ **FRP Grid Bonded to a Plate**



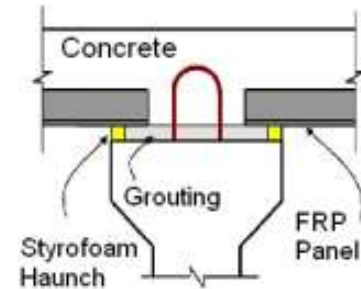
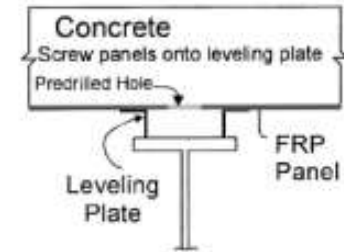
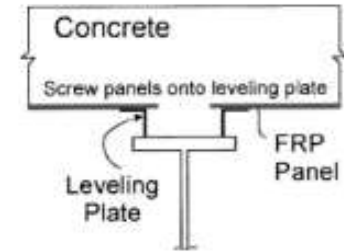
→ **Ribbed Plate**



→ **Dual Cavity System**



→ **Corrugated Plate Formwork**

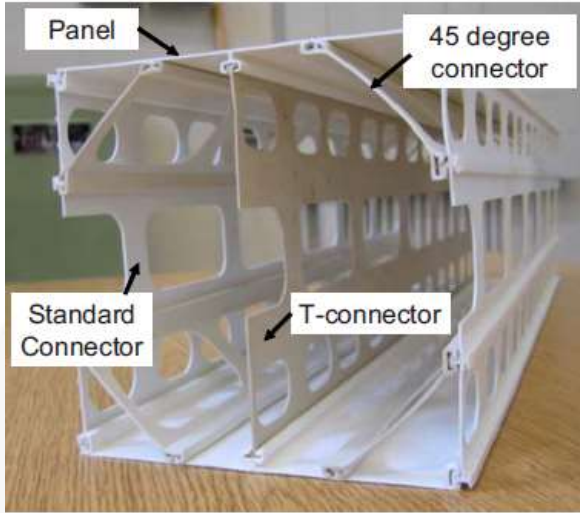


Effect of PVC Stay-In-Place Formwork on Mechanical Performance of Concrete

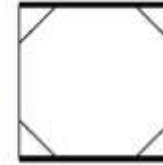
JOURNAL OF MATERIALS IN CIVIL ENGINEERING © ASCE / JULY 2009.



Katherine G. Kuder¹; Rishi Gupta²; Corinne Harris-Jones³; Richard Hawksworth⁴; Sean Henderson⁵; and Jason Whitney⁵

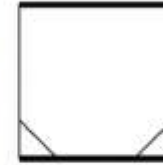
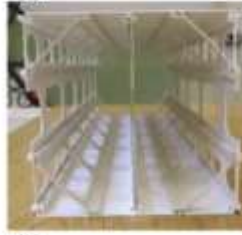
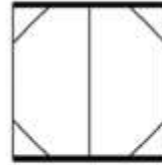


Octaform cell



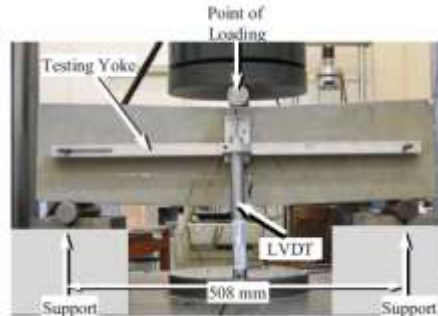
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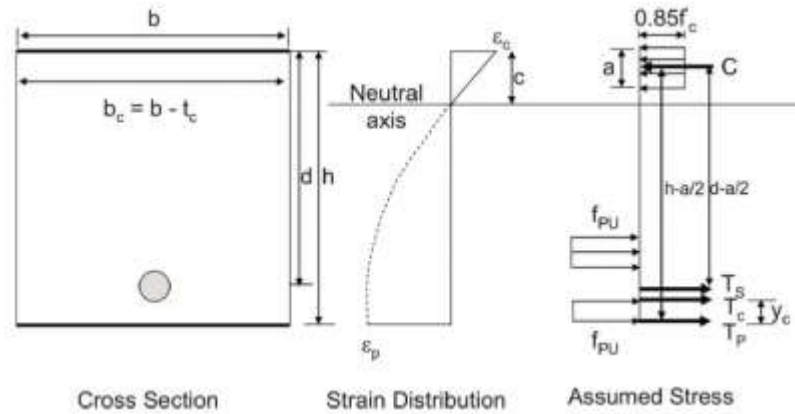
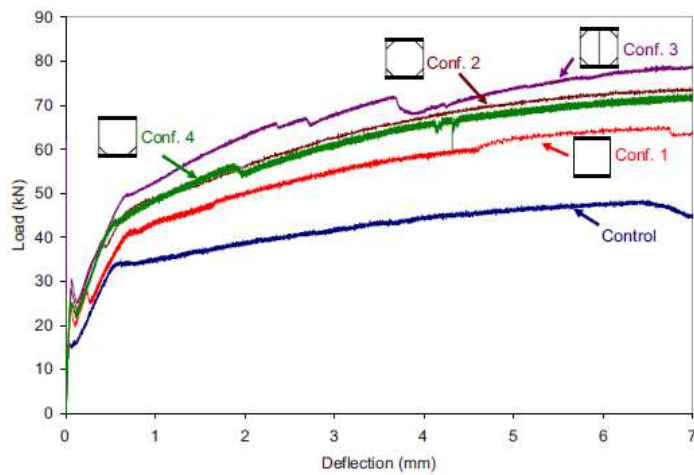
(b)



(c)

(d)





$$C = 0.85f'_c ab_c \quad (1)$$

$$T_s = A_s f_y \quad (2)$$

$$T_c = A_c f_{pu} \quad (3)$$

$$T_p = A_p f_{pu} \quad (4)$$

By equilibrium, the depth of the concrete stress block is

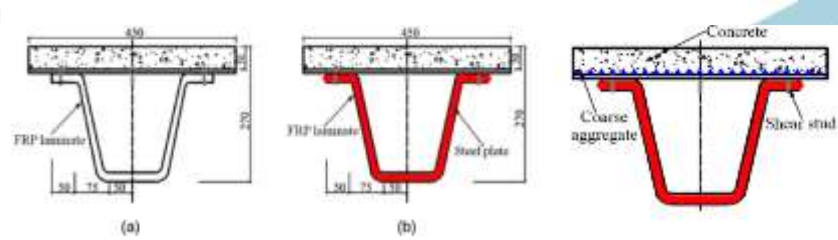
$$a = \frac{(A_c + A_p)f_{pu} + A_s f_y}{0.85f'_c ab_c}$$

$$M_n = A_s f_y \left(d - \frac{a}{2} \right) + A_p f_{pu} \left(h - \frac{a}{2} \right) + A_c f_{pu} \left(h - y_c - \frac{a}{2} \right)$$

Fracture Mechanism and Damage Evaluation of FRP/Steel–Concrete Hybrid Girder Using Acoustic Emission Technique

Fangzhu Du¹; Dongsheng Li²; and Yunyu Li³

J. Mater. Civ. Eng., 2019, 31(7): 04019111



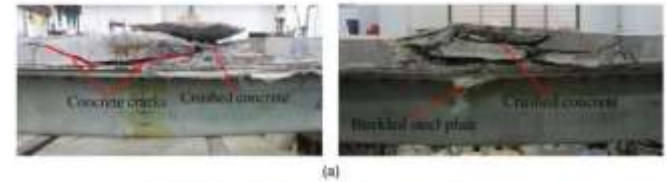
Specimen Details



Test Setup



Failure Pattern

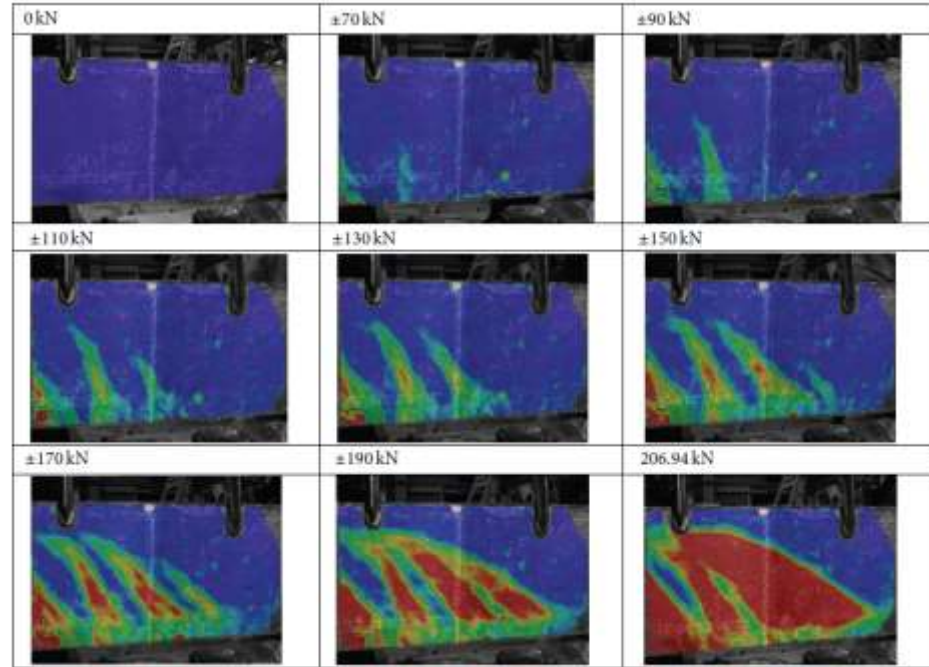
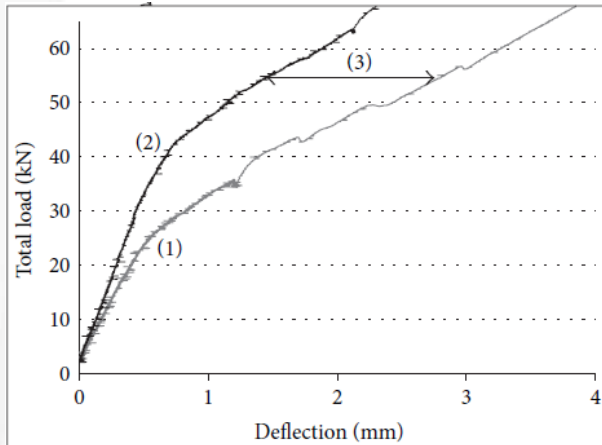
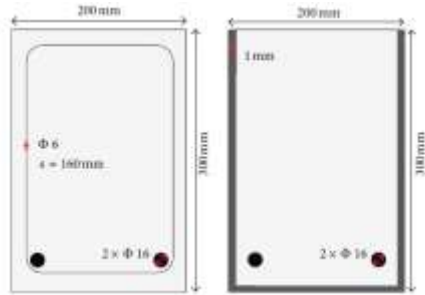


Failure Pattern

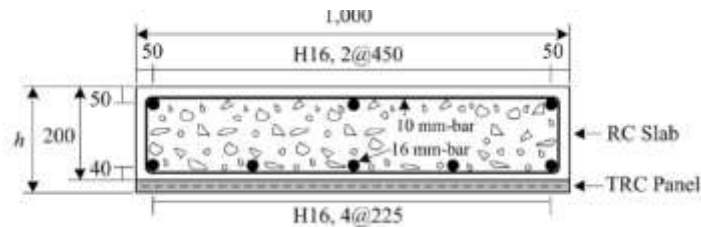
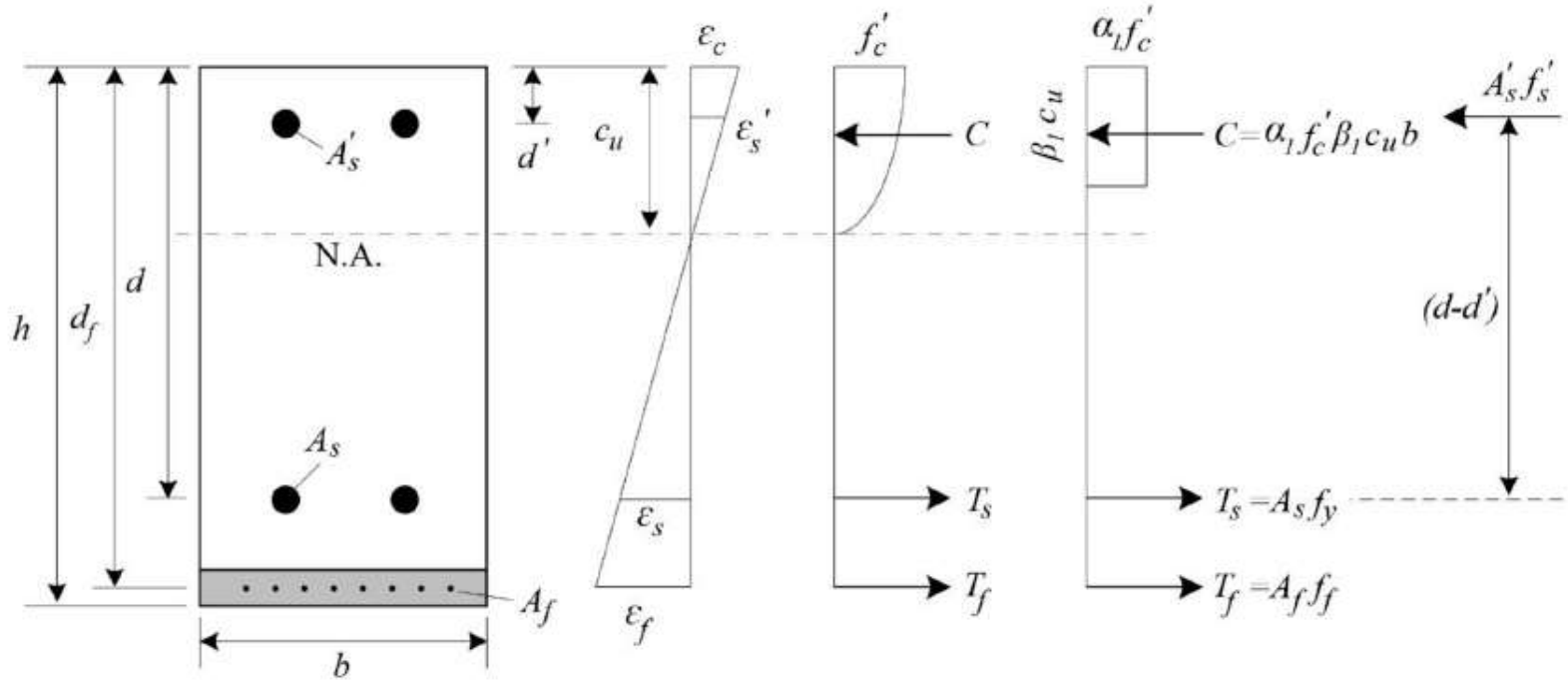
Stay-in-Place Formwork of TRC Designed as Shear Reinforcement for Concrete Beams

SIP - Textile Reinforced Concrete

S. Verbruggen, O. Remy, J. Wastiels, and T. Tysmans

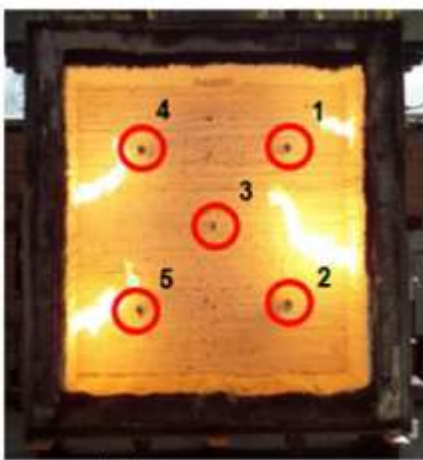
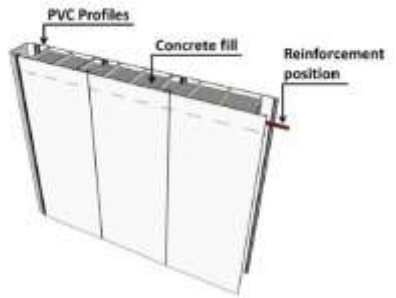


Internal Stress and Strain Distributions of RC Element casted on TRC -SIP

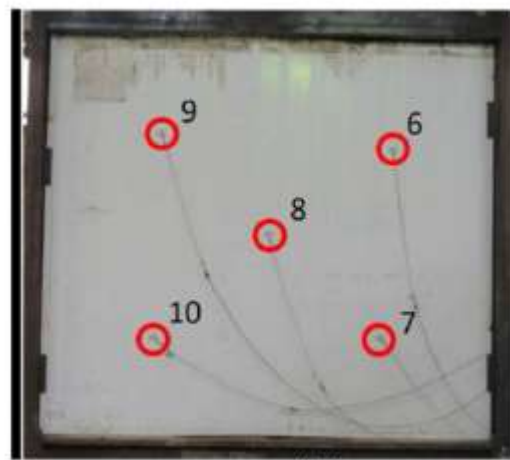


Fire resistance performance of concrete-PVC panels with polyvinyl chloride (PVC) stay in place (SIP) formwork

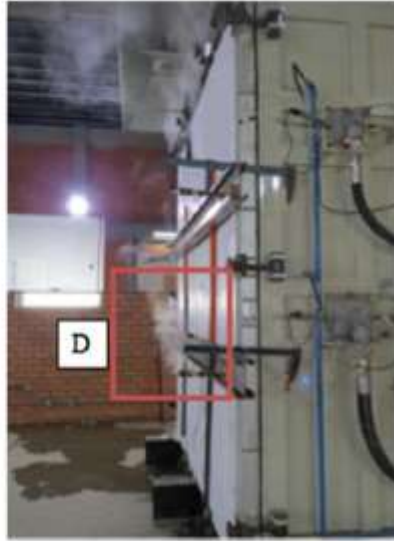
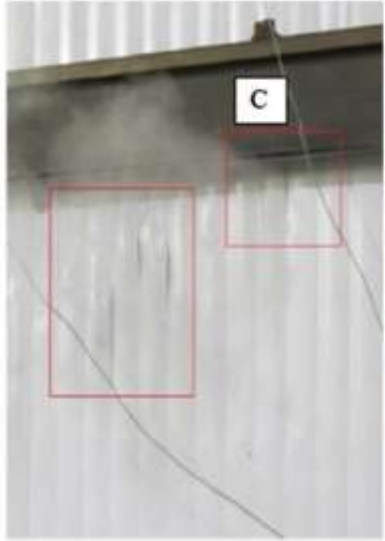
Michel Murillo A.^{1,2,3,4}, Bernardo F. Tutikian¹, Vinicius Ortolan⁵, Marcos L.S. Oliveira⁶, Carlos H. Sampaio⁷, Leandro Gómez P⁸, Luis F. Silva O⁴









(a)



(b)



Sample	Before exposure to fire	After exposure to fire
PVC1		
PVC2		
PVC3		

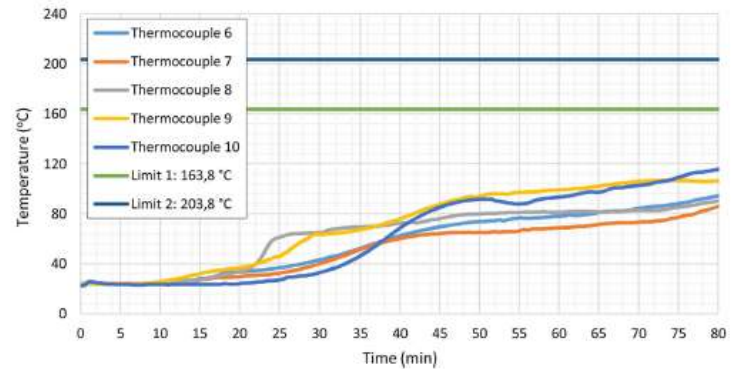


Fig. 9 – Temperature measurements recorded by the thermocouples on the external face of the PVC2 sample.

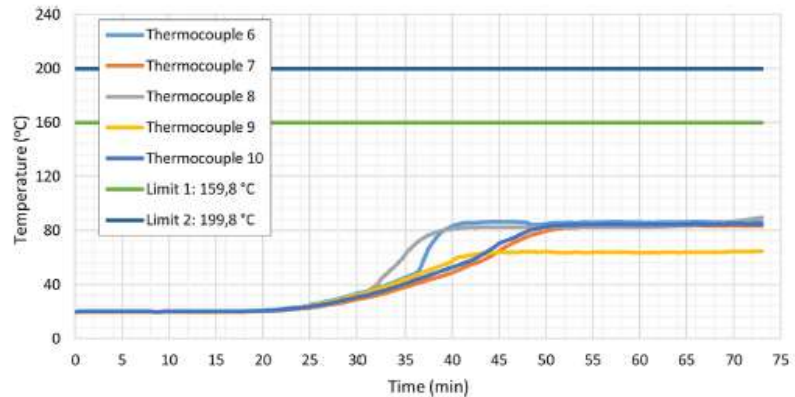


Fig. 10 – Temperature measurements recorded by the thermocouples on the external face of the PVC3 sample.

Lateral Pressure on Wall Formwork



$$P_m = C_w C_c [150 + 9000R / T]$$

lateral pressure for wall having the placement height less than or equal to $14 f_t$ having rate of placement less than $7f_t/hr$.

P_m = maximum lateral pressure, **lb/sqft**

C_w = unit weight coefficient

C_c = chemistry coefficient

R = rate of fill of concrete in form, **f_t/hr**

T = temperature of concrete in form, °F



For all wall forms with concrete placement rate from 7 to 15 f/hr , and for walls where the placement rate is less than 7 f/hr and the placement height exceeds 14 ft.

$$P_m = C_w C_c [150 + 43400 / T + 2800R / T]$$



Thank you

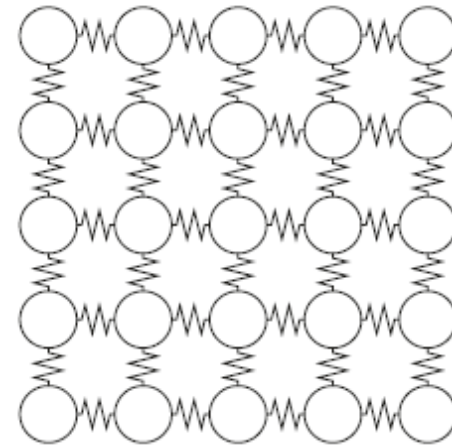


Outline of Presentation

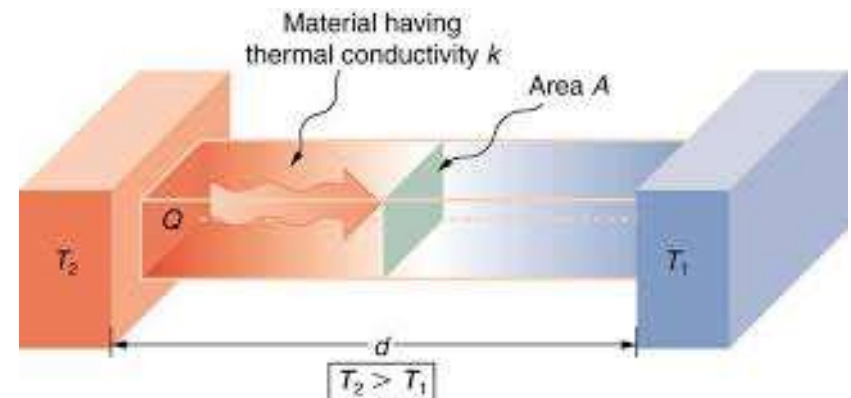


- 1 Steady and unsteady Heat Flow through Buildings
- 2 Thermal Admittance and decrement factor
- 3 Mean temperature in the space
- 4 Fluctuating Heat gains and Internal temperature
- 5 ECBC Codal Provisions & expt. Evaluation
- 6 Temperature Monitoring in Building-A case Study

- Heat transfer by conduction involves transfer of energy within a material **without any motion of the material as a whole**.
- The rate of heat transfer depends upon the **temperature gradient** and the **thermal conductivity** of the material.



Particles are held together very closely by strong electromagnetic forces

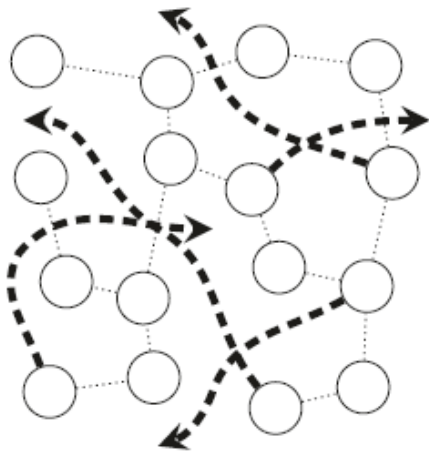




Heat Transfer-Convection



- Heat transfer by **mass motion of a fluid** such as **air or water** when the heated fluid is caused to move away from the source of heat, carrying energy with it.
- Convection above a hot surface occurs because **hot air expands, becomes less dense**. Hot water is likewise less dense than cold water and rises, **causing convection currents which transport energy**.



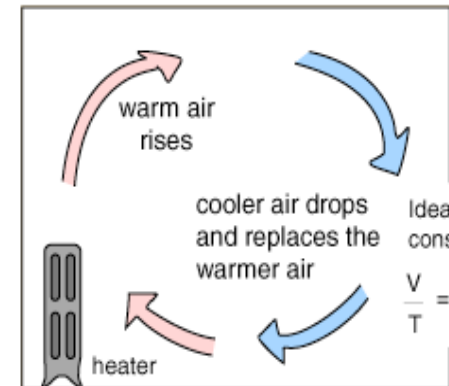
Particles are quite close to each other and irregularly connected by weak electromagnetic forces that are easily broken and re-established.

If volume increases, then density decreases, making it buoyant.

$$\rho = \frac{m}{V}$$

$$\frac{V}{T} = \text{constant}$$

If the temperature of a given mass of air increases, the volume must increase by the same factor.



Ideal gas law for constant pressure

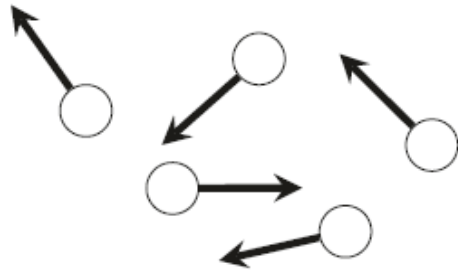
$$\frac{V}{T} = \frac{nR}{P} = \text{constant}$$



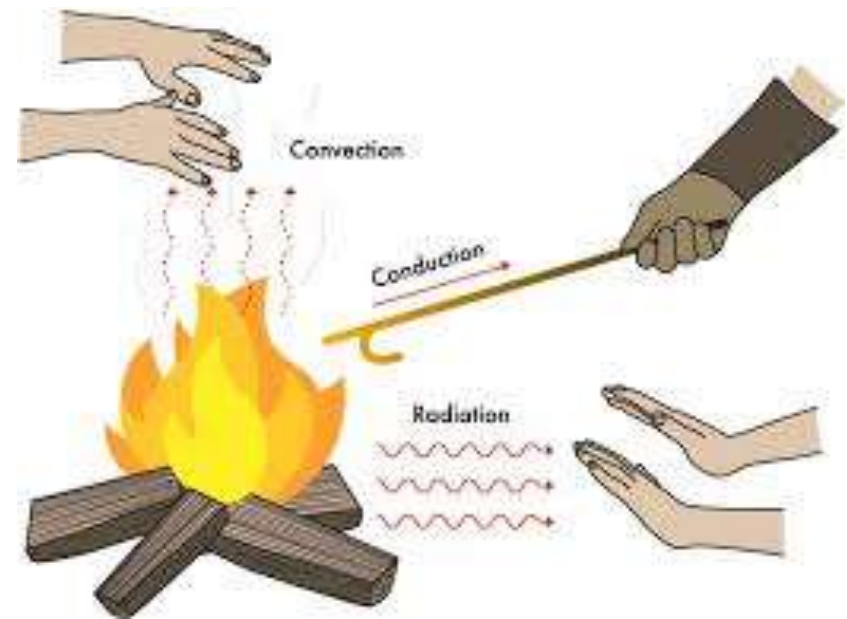
Heat Transfer- Radiation



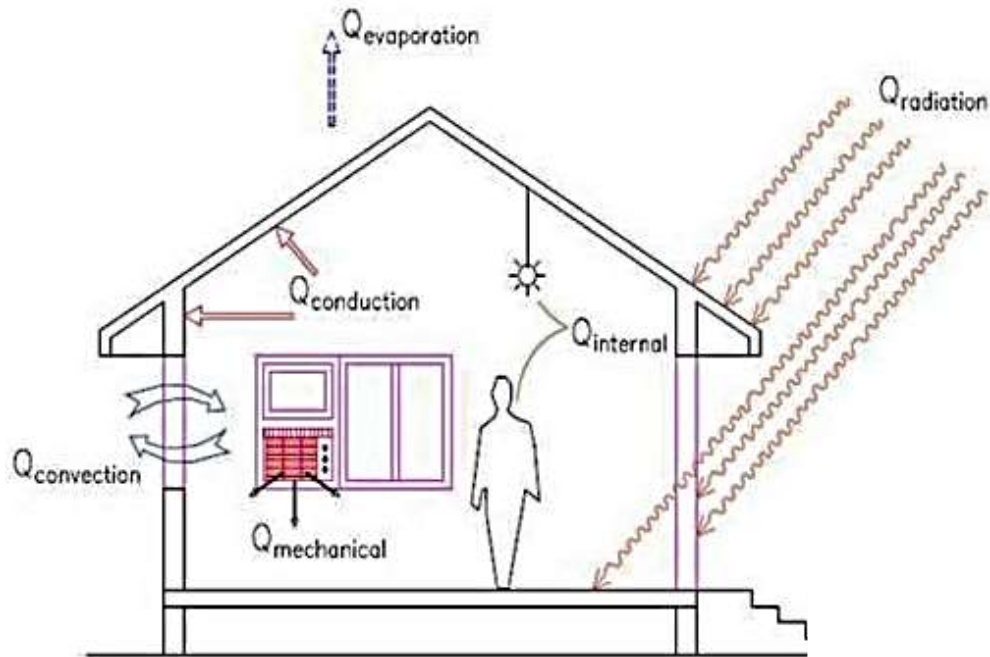
Radiation is heat transfer by the **emission of electromagnetic waves which carry energy away from the emitting object.**



There are no forces between them except for occasional collisions. They move around freely and quickly.



Heat Flow through Building Envelope



Q_s- Direct Solar radiation

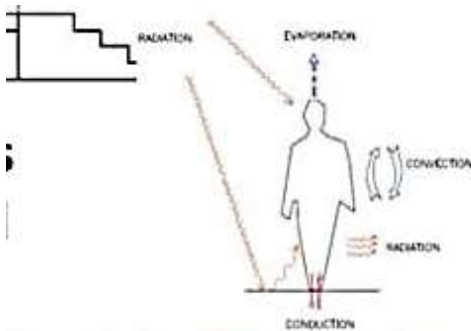
Q_c- heat flow through Conduction

Q_v- Heat flow through Ventilation

Q_i- heat generated through body, equipment's

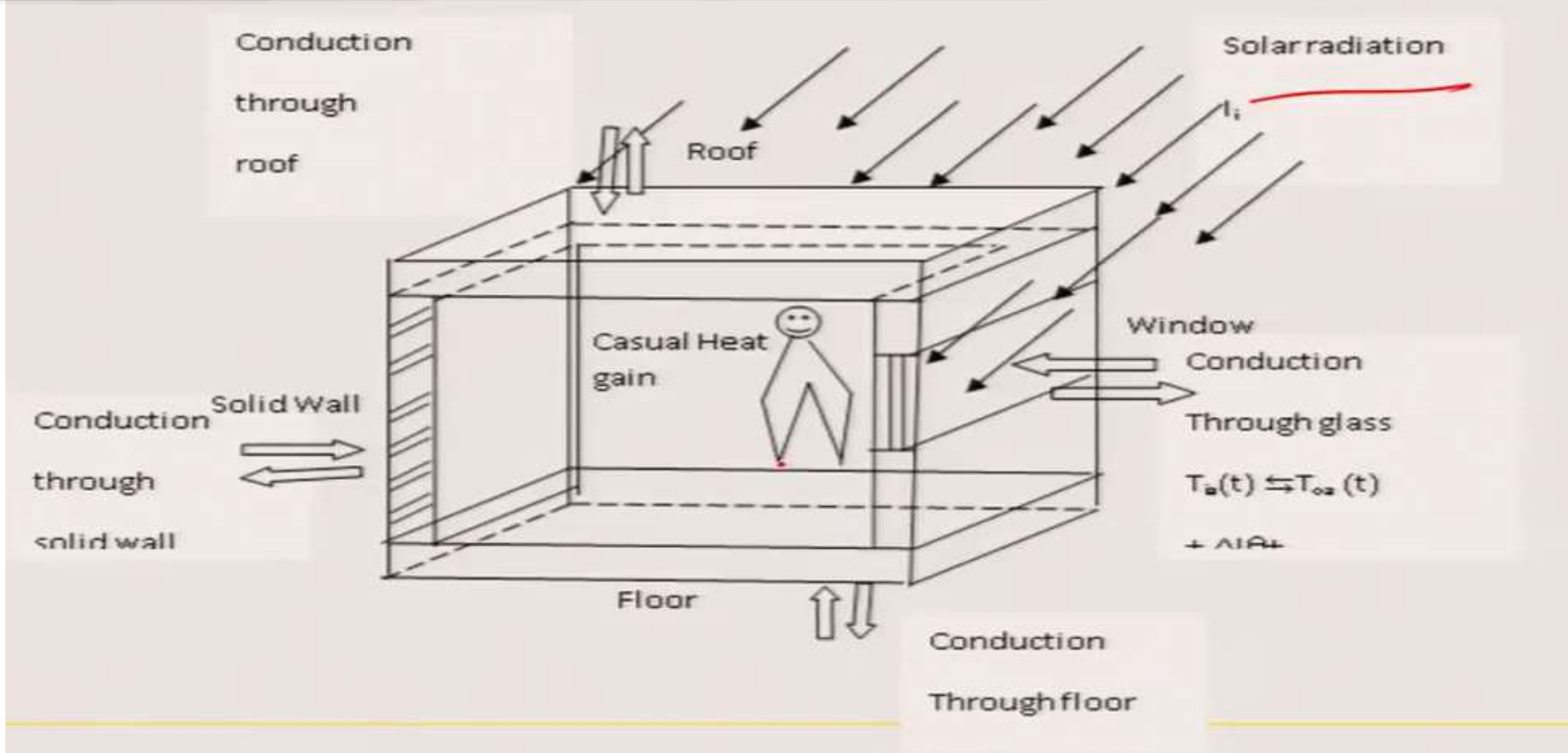
Q_e- Heat Evaporation/emission during night

Heat Exchange Processes Between A Building And External Environment



human body and the indoor environment

Heat Flow through Building Envelope



Q_s - Direct Solar radiation

Q_e - Heat Emission during night

Q_c - heat flow through Conduction

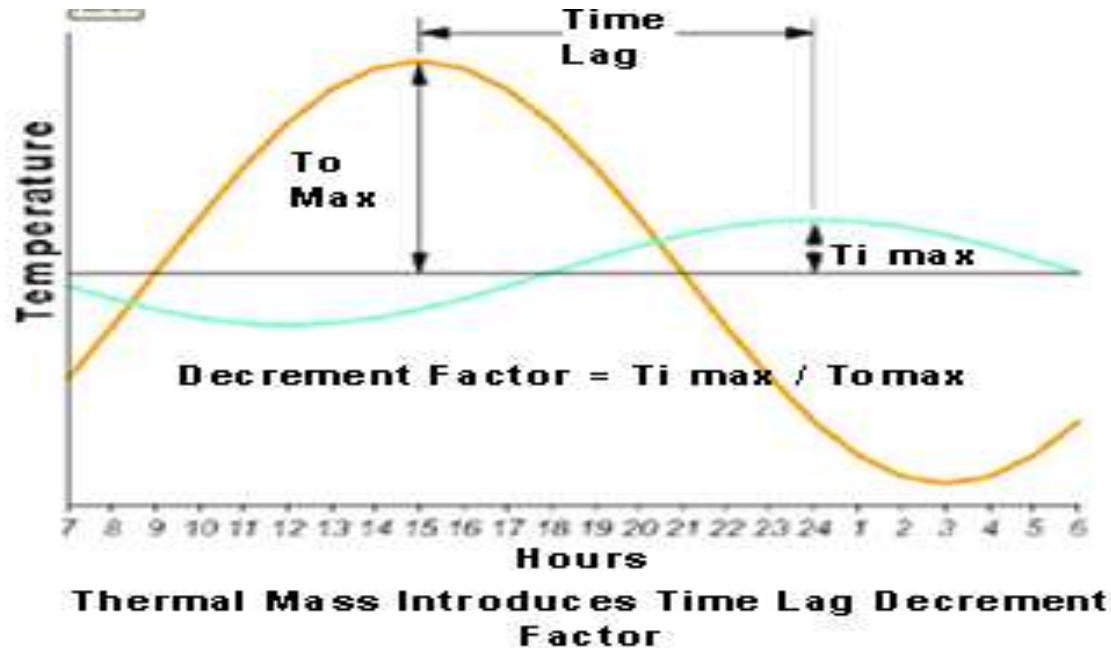
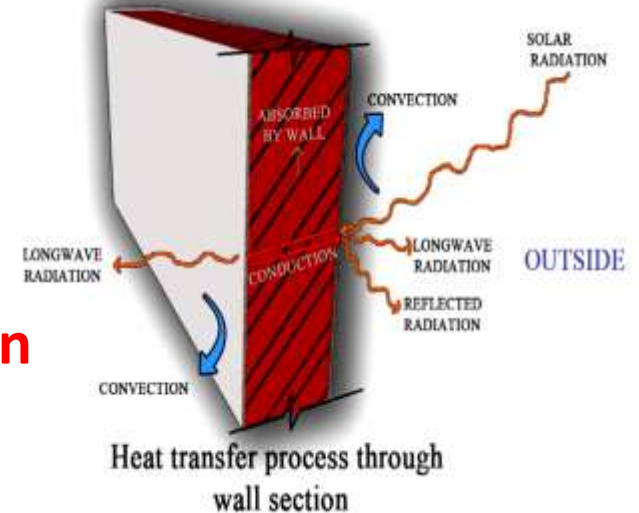
Q_v - Heat flow through ventilation

Q_i - heat generated through body, equipment's..

Heat Flow Path



- **Steady state: Temperature is constant at any time**
- **Transient Conduction/Dynamic /non-steady State)- Temperature at any location in a region changes with time**



HEAT CONDUCTION THROUGH A PLANE WALL



Let us consider a plane wall of homogeneous material through which heat is flowing in x-direction.,

Let,

L = thickness of the wall

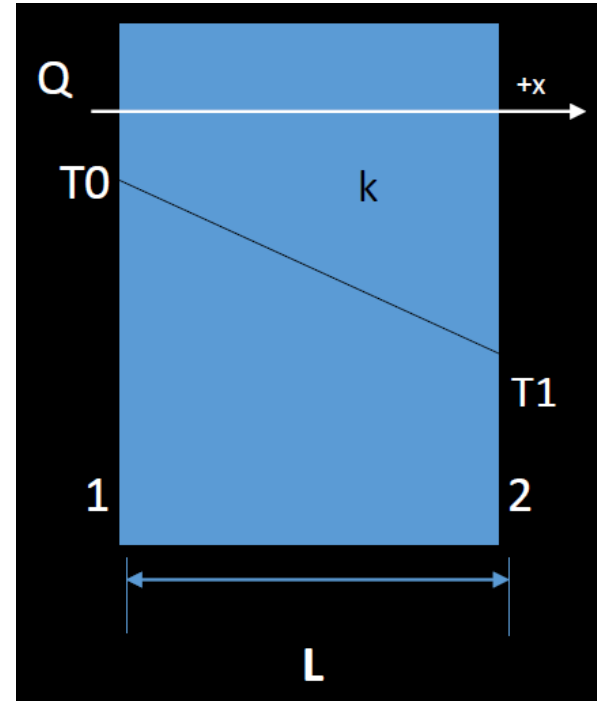
A = cross-sectional area of the wall

k = thermal conductivity of wall material

T_0, T_1 = temperature maintained at surfaces 1 and 2

ΔT - Temp difference inside and outside

α - Thermal diffusivity



HEAT CONDUCTION THROUGH A PLANE WALL



General heat conduction equation is:, (Fourier-Biot equation)

$$\partial^2 T / \partial x^2 + \partial^2 T / \partial y^2 + \partial^2 T / \partial z^2 + q/k = 1/\alpha * \partial T / \partial t$$

For one dimensional steady state system $(\partial T / \partial t) = 0$

With no heat generation $(q/k) = 0$

One dimensional flow , $\partial^2 T / \partial y^2 = \partial^2 T / \partial z^2 = 0$

Then, heat equation will be $\partial^2 T / \partial x^2 = 0$

$$d^2 T / dx^2 = 0$$

Integrating above equation,

$$dT / dx = C_1$$

Integrating it again,

$$T = C_1 x + C_2$$

Where C_1 and C_2 are arbitrary constants

Steady Heat Flow through wall



- At $x = 0$; $T = T_0$
- At $x = L$; $T = T_1$

From the expression derived above $T = C_1 \cdot x + C_2$ (1)

At $x = 0$;

$$T_0 = C_1 (0) + C_2$$

$$C_2 = T_0$$

At $x = L$;

$$T_1 = C_1 \cdot L + T_0$$

$$C_1 = (T_1 - T_0) / L$$

Eqn. 1 can be re-written as

$$T = (T_1 - T_0 / L) \cdot x + T_0$$

i.e temperature varies linearly with x

Steady Heat Flow through wall



- **Inference:**

1. **Temperature distribution across the wall is linear.**
2. **Temperature distribution is independent of k .**

From Fourier's Law of heat conduction, we have,

$$\text{Heat flow } Q = -k A dT/dx$$

$$dT/dx = d/dx ((T_1 - T_0)/L * x) + T_0 = (T_1 - T_0)/L$$

Fourier's Law can be re-written as,

$$Q = -k A (T_1 - T_0)/L$$

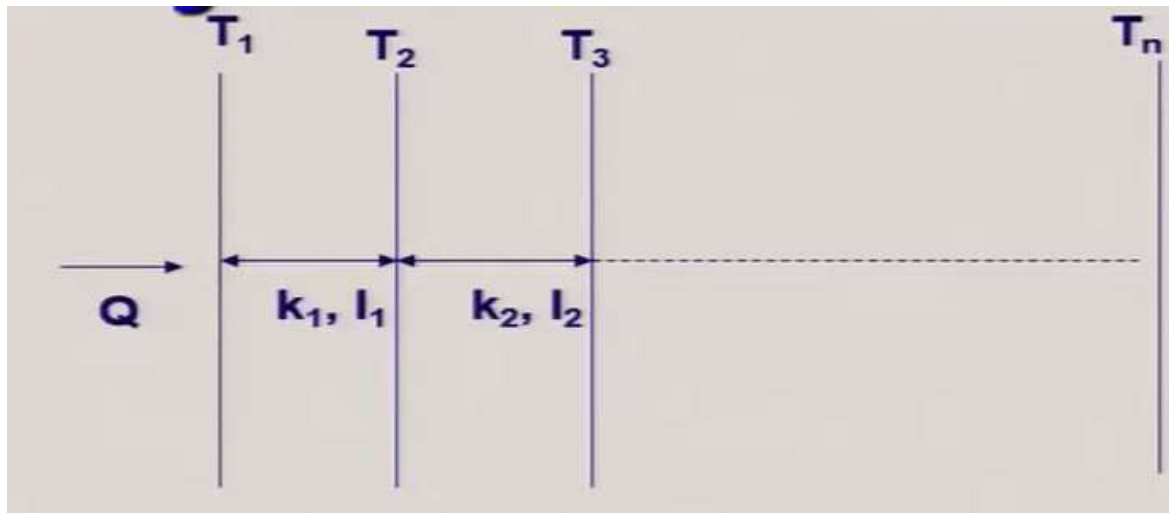
$$Q = -A U (T_1 - T_0)$$

Where, k - Thermal Conductivity W/mk

L/kA = Thermal Resistance of heat conduction (R) = (L/kA)

U - Thermal Transmittance, $W/m^2K = 1/R$

Steady Heat Flow through layered wall



Layers may include cavity or insulation. Cavity R is used

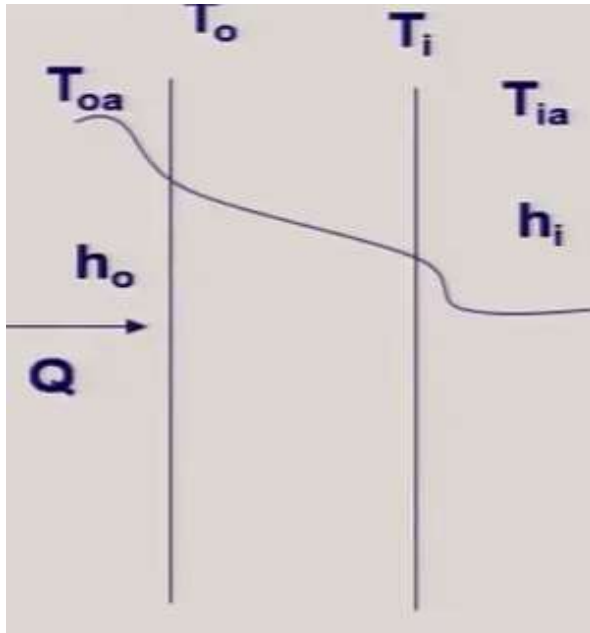
$$Q = k_1 A \frac{(T_1 - T_2)}{l_1} = k_2 A \frac{(T_2 - T_3)}{l_2} = \dots\dots\dots$$

$$T_1 - T_2 + T_2 - T_3 \dots\dots\dots T_n = Q/A [l_1/k_1 + l_2/k_2 + \dots\dots l_{n-1}/k_{n-1}]$$

$$T_1 - T_n = (Q/A) \times R$$

$$R = R_1 + R_2 + \dots\dots\dots$$

Steady Heat Flow through layered wall



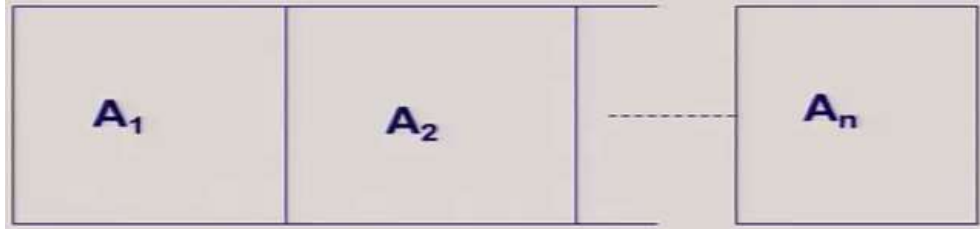
U - Thermal Transmittance, W/m^2K
h_o and *h_i* - Surface heat transfer coefficients

$$Q = h_o A (T_{oa} - T_o) = h_i A (T_i - T_{ia}) = (1/R) \times (T_o - T_i) A$$

$$1/U = 1/h_o + l_1/k_1 + l_2/k_2 + \dots + l_{n-1}/k_{n-1} + 1/h_i$$

$$Q = UA\Delta T$$

Steady Heat Flow through wall

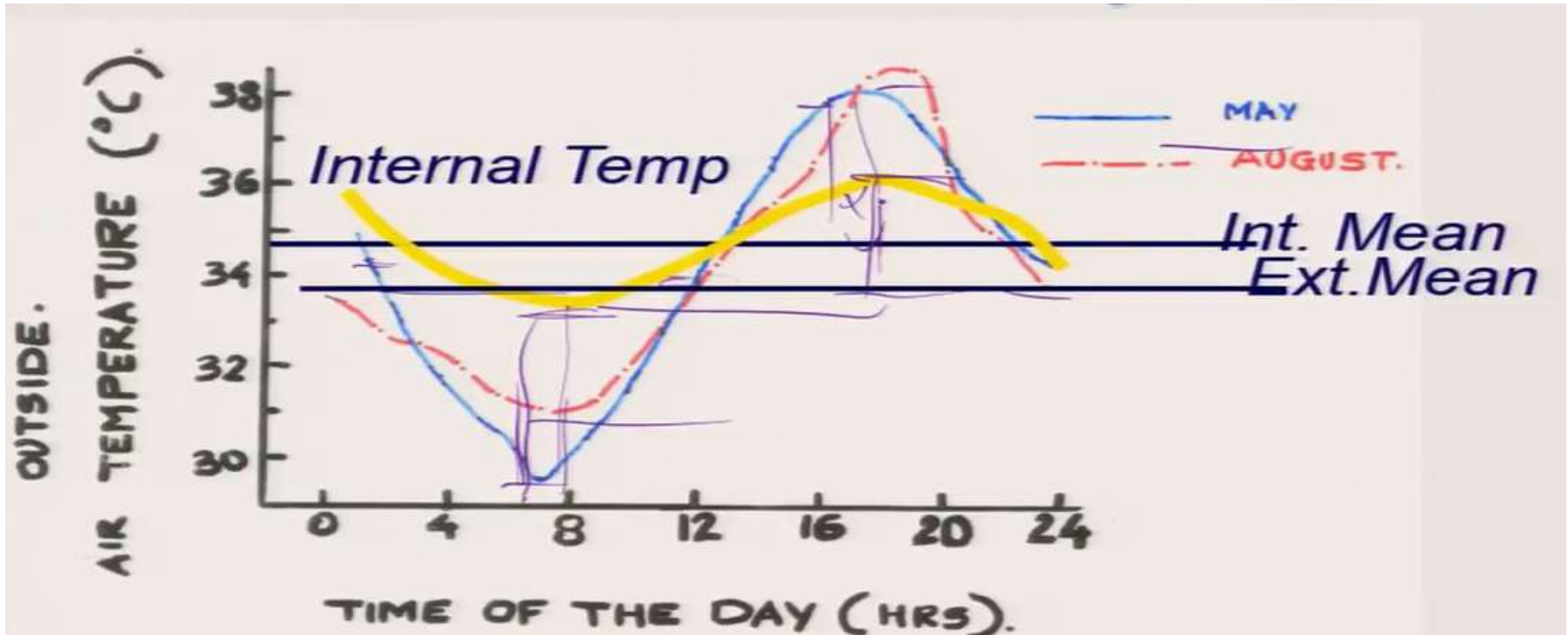


Different surfaces are exposed same temperature gradient

$$Q = [U_1 A_1 + U_2 A_2 \dots] (T_{oa} - T_{ia})$$

$$UA = [U_1 A_1 + U_2 A_2 \dots]$$

External and Internal Temperature



Due to periodic nature the temperature can be expressed as a mean temperature and a fluctuating component.

$$\text{i.e. } T_{oa}(t) = \bar{T}_{oa} + \text{fluctuation}$$

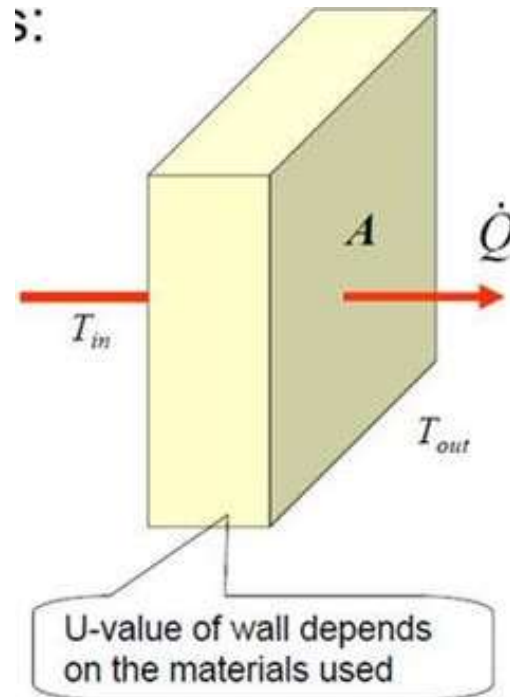
$$\& T_{ia}(t) = \bar{T}_{ia} + \text{fluctuation}$$

Steady Heat Flow



- For conducting in steady state, heat exchange (Q_{cd})

$$Q_{cd} = \sum U_j A_j (T_{oa} - T_{ia})$$



Effect of Radiation on opaque surface



- For unit area, heat absorbed by a surface = αI

After reaching steady state temperature (say at equivalent temperature t_{oe}),

The Heat Absorbed = Heat Dissipated

- i.e. $\alpha I = h_o (T_{oe} - T_{oa})$

$\alpha I / h_o = \text{Sol-air excess}$

$$T_{oe} = T_{oa} + \alpha I / h_o$$

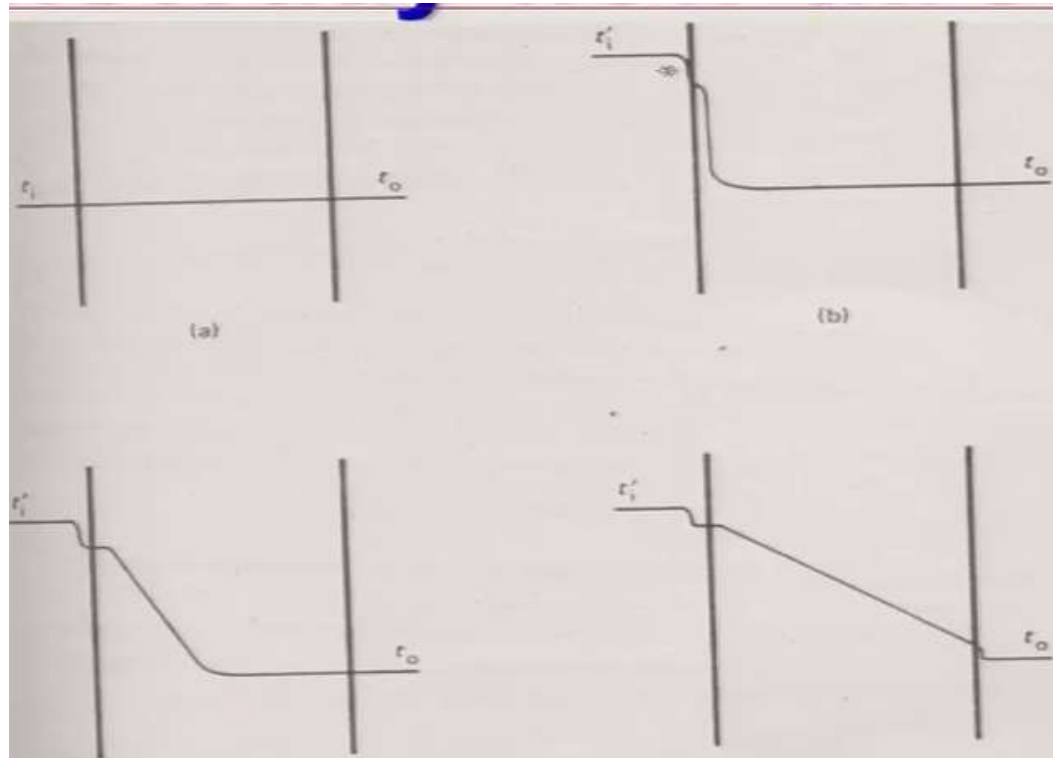
$\alpha = \text{Absorptivity of surface}$

$T_{oe} = \text{Sol-air temperature}$

$T_{oa} = \text{Outside air temperature}$

$h_o = \text{surface heat transfer coefficient}$

Temperature Gradient at different times

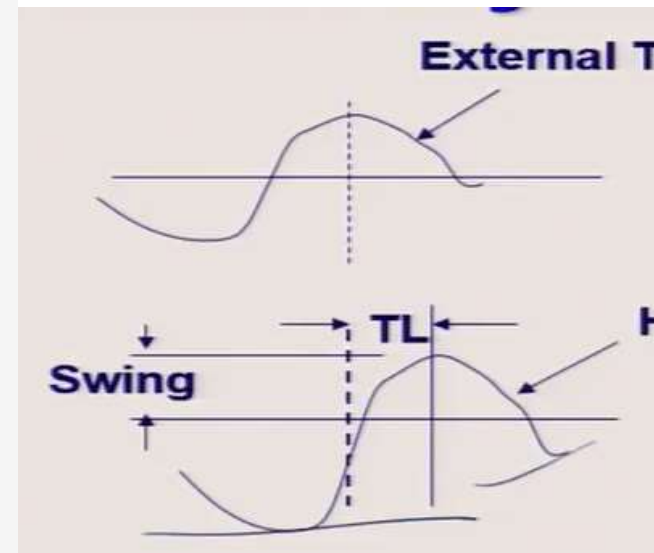
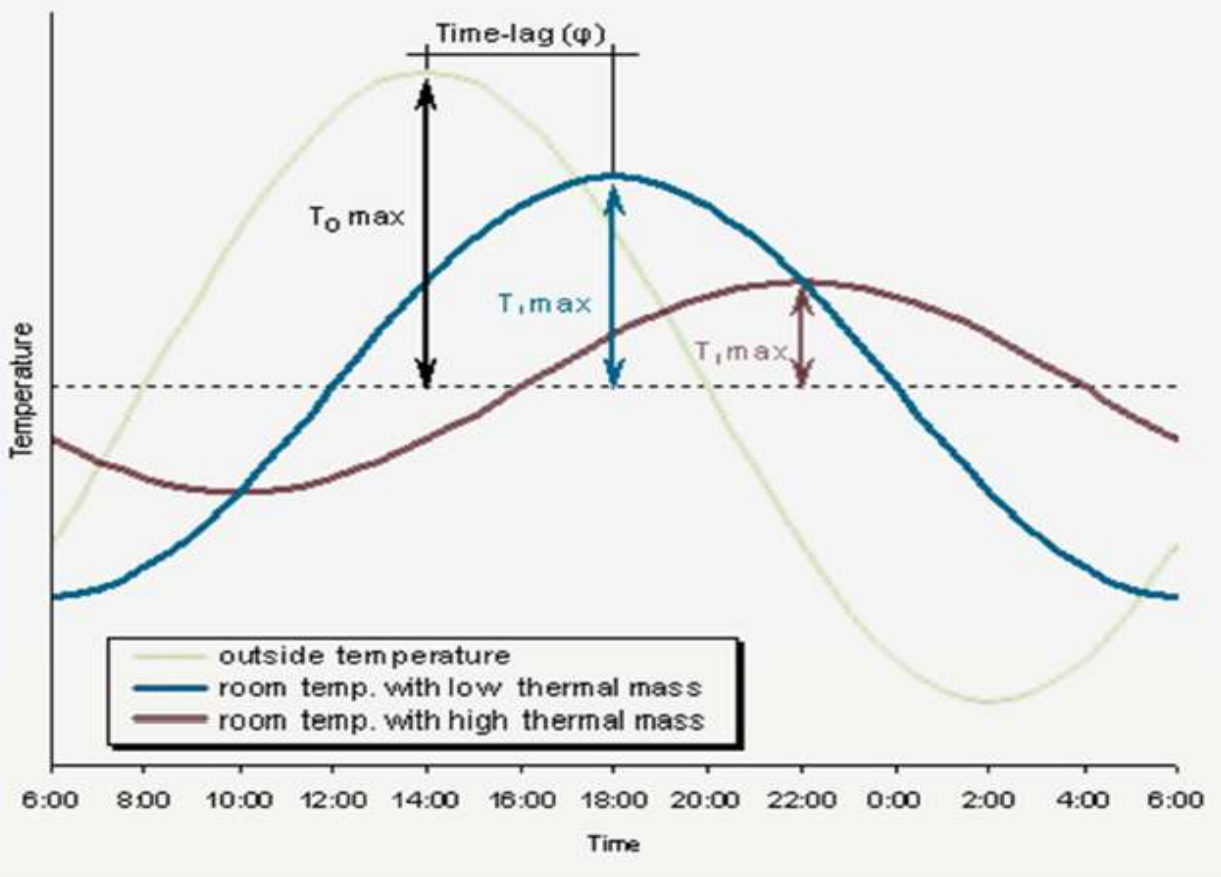


In (a) Temperature within the system does vary with time

In (b-d) Due to heat storage capacity of material

Unsteady flow occur

Unsteady Heat Flow through wall



a) Light wall

b) Heavy wall

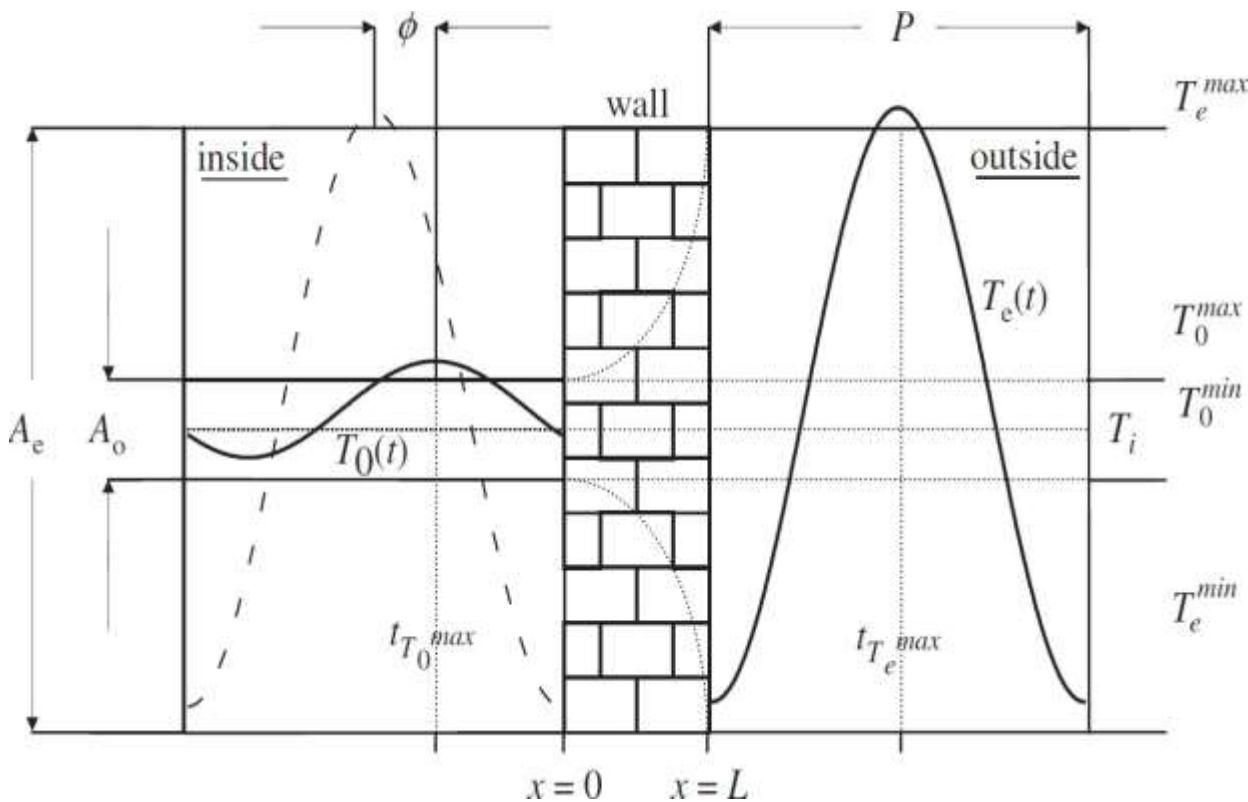
**TL: Time lag & Swing depends on thermal capacity i.e.,
Density x Specific heat**

Thermal Mass



- Thermal mass is a term used in solar passive design to describe materials that have **the ability to absorb and store heat.**
- Solar efficient homes incorporate thermal mass in order to remain warm overnight and through periods of cold or cloudy weather
- High density materials such **concrete, bricks, and tiles** require a great deal of heat energy to change their temperature and are therefore said to have high thermal mass. **Lightweight materials, on the other hand, such timber, have low thermal mass.**

Time Lag ϕ and Decrement factor f



Important characteristics to determine the heat storage capabilities of any material

The time (hour, h) it takes for the heat wave to propagate from the outer surface to the inner surface is named as “time lag (ϕ)” and the decreasing ratio of its amplitude during is named as “decrement factor (f)”

Where,

$t_{T_0^max}$ time in hours when **inside** surface temperatures are at their maximums,

$t_{T_e^max}$ time in hours when **outside** surface temperatures are at their maximums

P (24 h) is the period of the wave

Source: H Asan (2006)

Time Lag ϕ and Decrement factor f



The time lag may be computed as follows

$$\phi = \begin{cases} t_{T_o}^{\max} > t_{T_e}^{\max} \Rightarrow t_{T_o}^{\max} - t_{T_e}^{\max}, \\ t_{T_o}^{\max} < t_{T_e}^{\max} \Rightarrow t_{T_o}^{\max} - t_{T_e}^{\max} + P, \\ t_{T_o}^{\max} = t_{T_e}^{\max} \Rightarrow P, \end{cases}$$

The decrement factor is defined as:

$$f = \frac{A_o}{A_e} = \frac{T_o^{\max} - T_o^{\min}}{T_e^{\max} - T_e^{\min}}$$

Where,

A_o , A_e amplitudes of the wave in the inner & outer surfaces of the wall

Smaller the decrement factor, the more effective is the envelope at suppressing temperature swings.

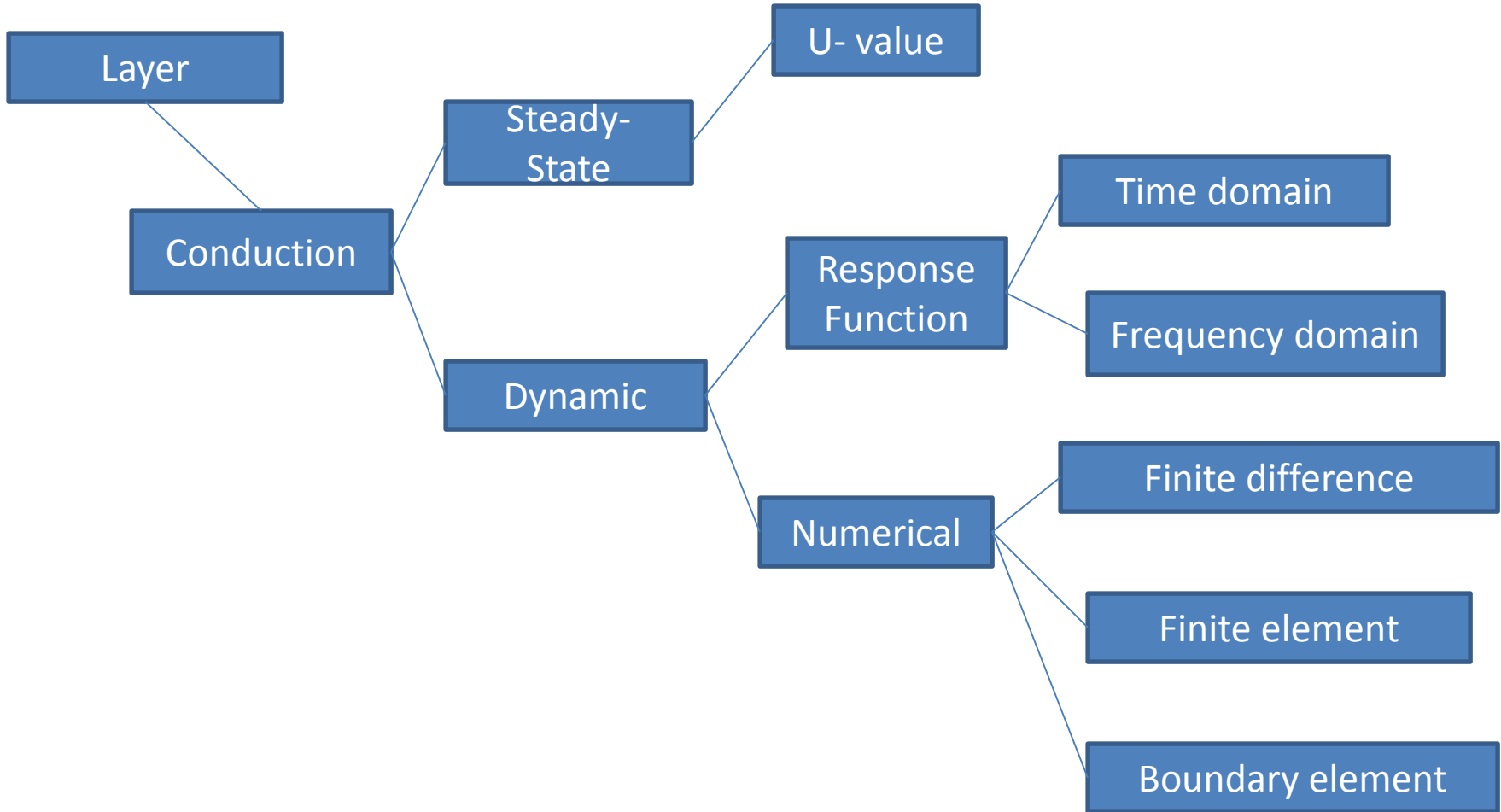
The time lag of the heat wave should be as high as possible to delay an outside sinusoidal heat wave from entering into the room through the wall or roof.

Thermal Performance



- Effect of radiation on opaque surface is taken account of **through an equivalent temperature**
- **Short wave absorptivity (Low) and long wave emissivity (High) are also important**
- Sequence of layer does not influence steady flow although **may have effect in periodic heat flow**

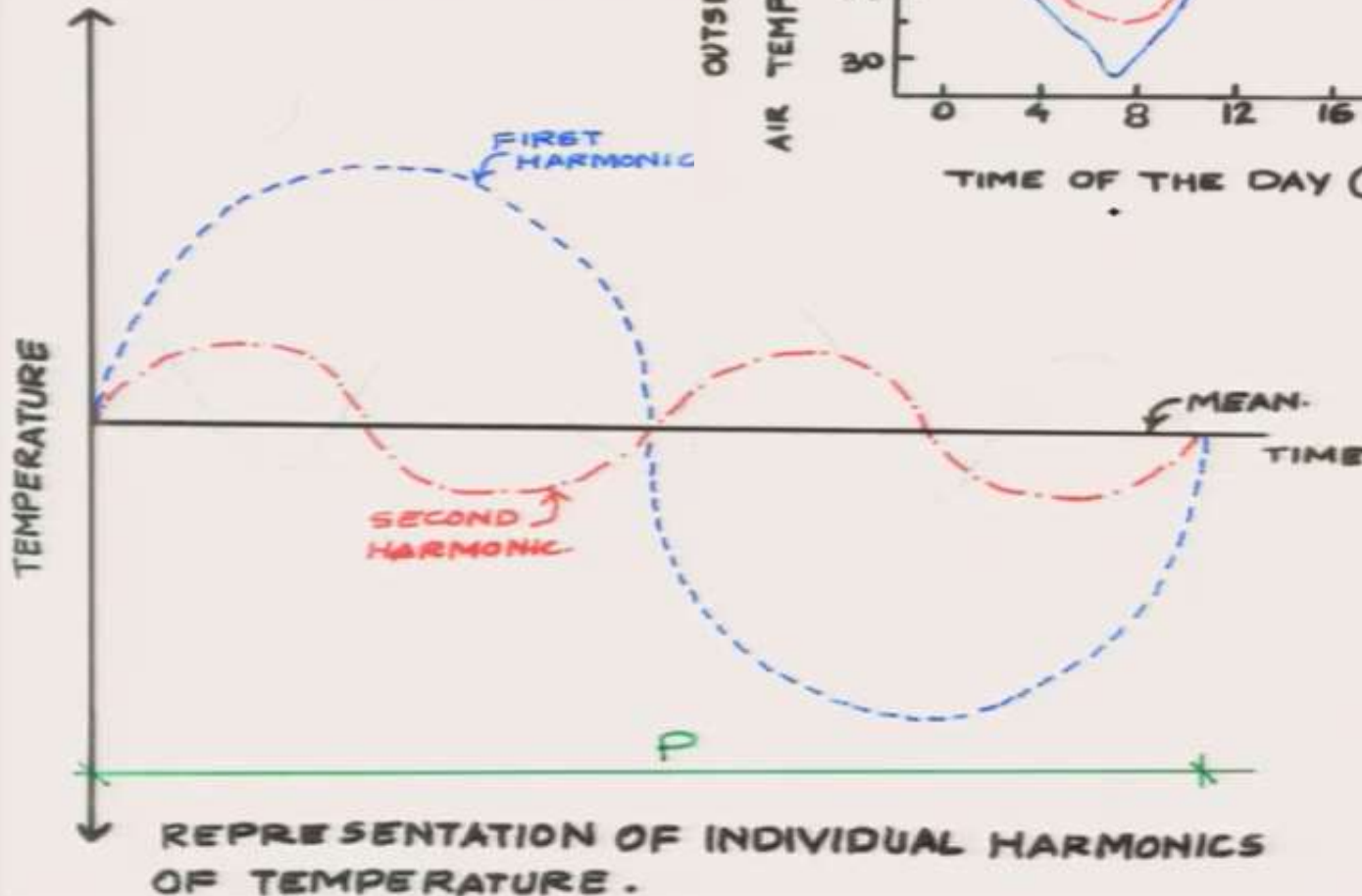
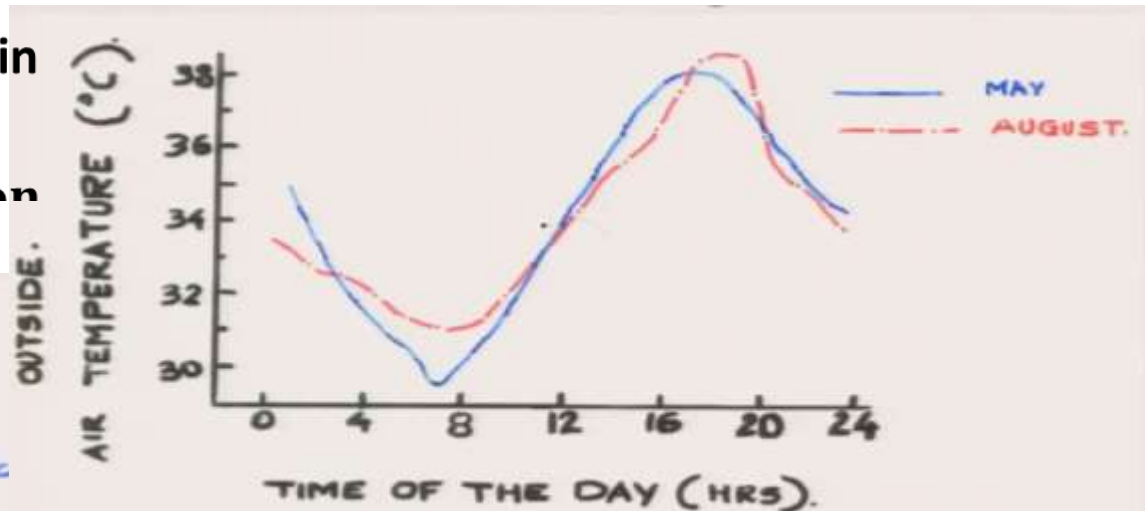
Heat Flow through Building



Harmonics



- Can be calculated by sum of sin and cosine functions...
- Fourier series of Expansion



Frequency Domain Treatment



$$T(t) = \bar{T} + \sum_{j=1}^{\infty} \left[a_j \cos\left(\frac{2\pi j}{p}t\right) + b_j \sin\left(\frac{2\pi j}{p}t\right) \right]$$

\bar{T} is the mean.

j corresponds to a harmonic

P is period of the fundamental (2π)

$$T(t) = \bar{T} + \sum_{j=1}^{\infty} T_j \cos(\omega_j t + \phi_j)$$

ω = angular frequency = $\left(\frac{2\pi j}{p}\right)$

And ϕ is $\tan^{-1}\left(-\frac{b_j}{a_j}\right)$

Frequency Domain Treatment



a_j, b_j can be determined by multiplying $\cos\left(\frac{2\pi jt}{p}\right)$ and $\sin\left(\frac{2\pi jt}{p}\right)$

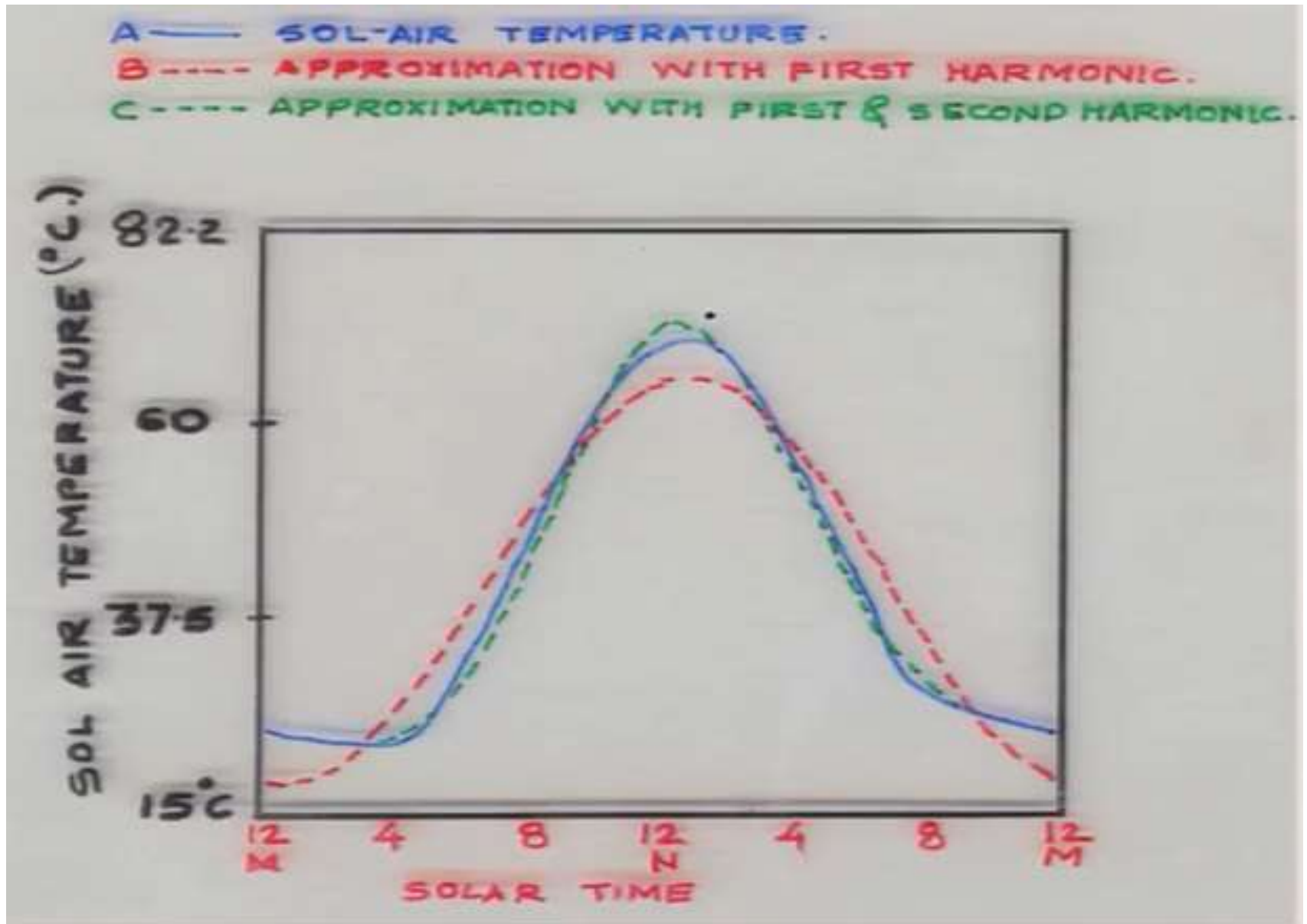
$$a_j = \frac{2}{p} \int_{-p/2}^{p/2} T(t) \cos\left(\frac{2\pi jt}{p}\right) dt$$

$$b_j = \frac{2}{p} \int_{-p/2}^{p/2} T(t) \sin\left(\frac{2\pi jt}{p}\right) dt$$

$$\bar{T} = \frac{1}{p} \int_{-p/2}^{p/2} T(t) dt$$

$$T_j = (a_j^2 + b_j^2)^{1/2}, \quad \phi = \tan^{-1}\left(-\frac{b_j}{a_j}\right)$$

Daily Temperature Variation



Unsteady Heat Flow through wall



The steady flow deal by simple eq. $Q = UA\Delta T$

$$\frac{\partial T(x, t)}{\partial x} = -\frac{1}{k} q(x, t)$$

$q_{in} - q_{out}$ through unit area in 1-D situation is the rate at which heat is stored in $1 \times dx$ volume

$$\frac{\partial T(x, t)}{\partial x} = -\rho c \frac{\partial T}{\partial t}$$

Temp function of Time and space

$$\frac{\partial^2 T(x, t)}{\partial x^2} = \frac{\rho c}{k} \frac{\partial T(x, t)}{\partial t} = \frac{1}{\alpha} \frac{\partial T(x, t)}{\partial t}$$

Diffusivity $\alpha = \frac{k}{\rho c} \text{m}^2/\text{s}$

ρ – Density ; c – specific heat (J/°C/kg)

Second order Differential equation

To solve this, many techniques, Numerical such as FDM, FE, FVM or Frequency domain solutions done with Laplace transformation...

Unsteady Heat Flow through wall



$$L [T(x, t)] = \int_0^{\infty} e^{-st} T(x, t) dt$$

LT is essentially converting Time domain in to domain of 's' variable

$$\frac{\partial^2 L [T(x, t)]}{\partial x^2} = \frac{s}{\alpha} L[T(x, t)] - T(x, 0)$$

Putting initial condition at $t=0$, $T(x, 0)=0$ & $L[T(x, t)]=\theta$, the Ordinary differential equation in θ is

$$\frac{\partial^2 \theta}{\partial x^2} = \frac{s}{\alpha} \theta$$

Unsteady Heat Flow through wall



Solving the ODE, solution is obtained in θ & inverse transform gives the solution

Solving the auxiliary equation

$$D^2 = \frac{s}{\alpha}, \quad D = \pm \sqrt{\frac{s}{\alpha}} = \pm p$$

$$\theta = Ae^{-px} + Be^{px} \text{ (General solution)}$$

$$\frac{d\theta}{dx} = -pAe^{-px} + pBe^{px}$$

$$\text{For } x=0, \theta = \theta_0, \phi = \phi_0 = -k \left(\frac{d\theta}{dx} \right) \text{ (Defined)}$$

$$\theta_0 = A + B$$

$$\phi_0 = kpA - kpB$$

Unsteady Heat Flow through wall



$$\theta_0 = A + B \dots\dots\dots 1$$

$$\phi_0 = kpA - kpB \dots\dots\dots 2$$

Solving above two equations...

$$A = \frac{1}{2} \left[\theta_0 + \frac{\phi_0}{kp} \right]$$

$$B = \frac{1}{2} \left[\theta_0 - \frac{\phi_0}{kp} \right]$$

Unsteady Heat Flow through wall



θ & Φ can be rewritten in terms of θ_0, Φ_0

$$\theta = \frac{1}{2} \left[\theta_0 + \frac{\Phi_0}{kp} \right] e^{-px} + \frac{1}{2} \left[\theta_0 - \frac{\Phi_0}{kp} \right] e^{px}$$

$$\theta = \frac{1}{2} \theta_0 [e^{-px} + e^{px}] + \frac{1}{2} \frac{\Phi_0}{kp} [e^{-px} - e^{px}]$$

By replacing

$$(e^{-px} + e^{px})/2 = \cosh-px \&$$

$$(e^{-px} - e^{px})/2 = -2\sinh-px$$

Unsteady Heat Flow through wall



$$\theta = \frac{1}{2} \theta_0 [e^{-px} + e^{px}] + \frac{1}{2} \frac{\phi_0}{kp} [e^{-px} - e^{px}]$$

Replacing, p , & using hyperbolic functions

$$\theta(x, s)$$

$$= \theta_0(0, s) \cosh \sqrt{\frac{s}{\alpha}} x - \frac{\phi_0(0, s)}{kp} \sinh \sqrt{\frac{s}{\alpha}} x$$

Unsteady Heat Flow through wall



Similarly for ϕ

$$\phi = -k \left(\frac{d\theta}{dx} \right) = kpAe^{-px} + kpBe^{px}$$

$$\phi = kp \frac{1}{2} \left[\theta_0 + \frac{\phi_0}{kp} \right] e^{-px} - kp \frac{1}{2} \left[\theta_0 - \frac{\phi_0}{kp} \right] e^{px}$$

$$\phi = -\frac{1}{2} kp \theta_0 [-e^{-px} + e^{px}] + \frac{1}{2} \phi_0 [e^{-px} + e^{px}]$$

Using hyperbolic functions

$$\phi(x, s) = -\theta_0(0, s)k \sqrt{\frac{s}{\alpha}} \sinh \sqrt{\frac{s}{\alpha}} x + \phi_0(0, s) \cosh \sqrt{\frac{s}{\alpha}} x$$

Unsteady Heat Flow through wall



Rewriting the equations again, i.e. x replaced by l

Equations are based on initial BC i.e. at $t=0$ $T(\text{temp})=0$

$$\theta(l, s) = \theta_0(0, s) \cosh \sqrt{\frac{s}{\alpha}} l - \frac{\phi_0(0, s)}{kp} \sinh \sqrt{\frac{s}{\alpha}} l$$

$$\phi(l, s) = -\theta_0(0, s) k \sqrt{\frac{s}{\alpha}} \sinh \sqrt{\frac{s}{\alpha}} l + \phi_0(0, s) \cosh \sqrt{\frac{s}{\alpha}} l$$

Unsteady Heat Flow through wall



In matrix form,

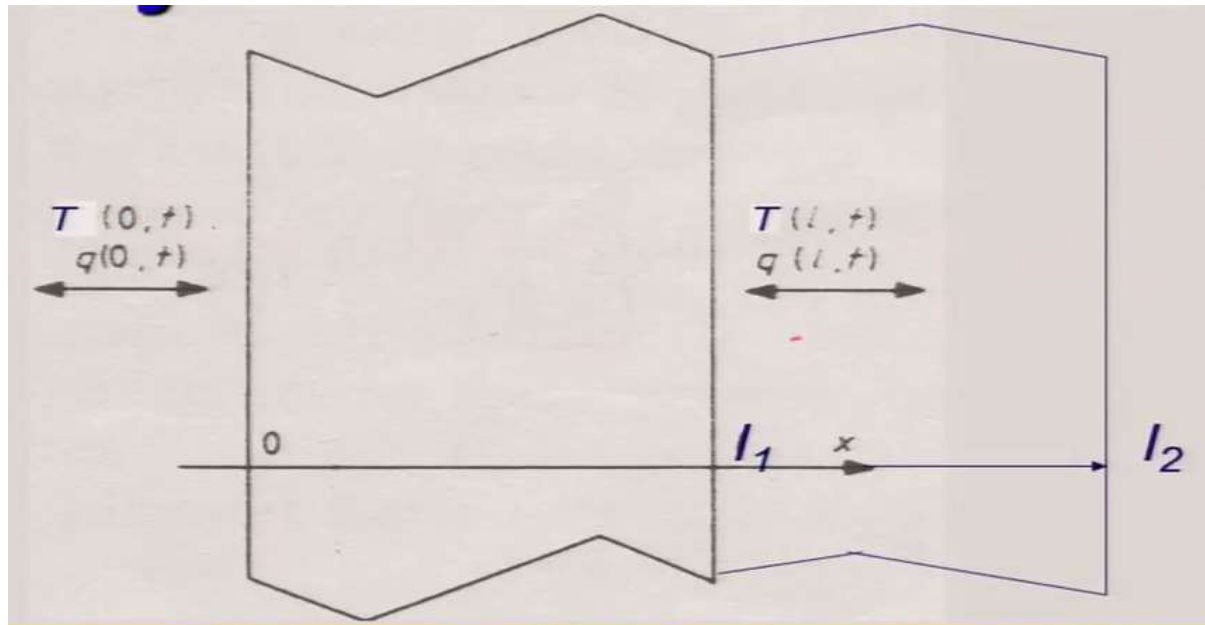
$$\begin{bmatrix} \theta(l, s) \\ \phi(l, s) \end{bmatrix} = \begin{bmatrix} m_{11} & m_{12} \\ m_{21} & m_{22} \end{bmatrix} \begin{bmatrix} \theta(0, s) \\ \phi(0, s) \end{bmatrix}$$

$$m_{11} = m_{22} = \cosh \sqrt{\frac{s}{\alpha}} l;$$

$$m_{12} = -\frac{1}{k \sqrt{\frac{s}{\alpha}}} \sinh \sqrt{\frac{s}{\alpha}} l$$

$$m_{21} = -k \sqrt{\frac{s}{\alpha}} \sinh \sqrt{\frac{s}{\alpha}} l$$

Unsteady Heat Flow through wall: Layered Construction



$$\begin{bmatrix} \theta(l_1, s) \\ \phi(l_1, s) \end{bmatrix} = \begin{bmatrix} m_{11}^1 & m_{12}^1 \\ m_{21}^1 & m_{22}^1 \end{bmatrix} \begin{bmatrix} \theta(0, s) \\ \phi(0, s) \end{bmatrix}$$

$$\begin{bmatrix} \theta(l_2, s) \\ \phi(l_2, s) \end{bmatrix} = \begin{bmatrix} m_{11}^2 & m_{12}^2 \\ m_{21}^2 & m_{22}^2 \end{bmatrix} \begin{bmatrix} \theta(l_1, s) \\ \phi(l_1, s) \end{bmatrix}$$

Unsteady Heat Flow through wall



$$\begin{bmatrix} \theta(l_2, s) \\ \phi(l_2, s) \end{bmatrix} = \begin{bmatrix} m_{11}^2 & m_{12}^2 \\ m_{21}^2 & m_{22}^2 \end{bmatrix} \begin{bmatrix} m_{11}^1 & m_{12}^1 \\ m_{21}^1 & m_{22}^1 \end{bmatrix} \begin{bmatrix} \theta(0, s) \\ \phi(0, s) \end{bmatrix}$$
$$\begin{bmatrix} \theta(L, s) \\ \phi(L, s) \end{bmatrix} = \begin{bmatrix} A & B \\ C & D \end{bmatrix} \begin{bmatrix} \theta(0, s) \\ \phi(0, s) \end{bmatrix}$$

$$\begin{bmatrix} A & B \\ C & D \end{bmatrix} = \begin{bmatrix} m_{11}^2 & m_{12}^2 \\ m_{21}^2 & m_{22}^2 \end{bmatrix} \begin{bmatrix} m_{11}^1 & m_{12}^1 \\ m_{21}^1 & m_{22}^1 \end{bmatrix} \dots$$

Unsteady Heat Transfer



For air layer ,

Thermal capacity of air layer is very small

Therefore, assume $\rho C \rightarrow 0$, & $\frac{k}{\rho C} = \alpha \rightarrow \infty$,

That mean it will allow heat to go instantaneously,

$$l \sqrt{\frac{s}{\alpha}} \rightarrow 0$$

$$m_{11} = m_{22} = \cosh \sqrt{\frac{s}{\alpha}} l \rightarrow 1$$

$$\lim_{\sqrt{\frac{s}{\alpha}} l \rightarrow 0}$$

Unsteady Heat Transfer



$$m_{12} = -\frac{1}{k\sqrt{\frac{s}{\alpha}}} \sinh \sqrt{\frac{s}{\alpha}} l = \frac{l}{k} - \frac{\sinh \sqrt{\frac{s}{\alpha}} l}{\sqrt{\frac{s}{\alpha}} l} = -\frac{l}{k} = -1/h$$

$\lim_{\sqrt{\frac{s}{\alpha}} l \rightarrow 0} \lim_{\sqrt{\frac{s}{\alpha}} l \rightarrow 0}$

For Air Layer

$$\begin{bmatrix} m_{11} & m_{12} \\ m_{21} & m_{22} \end{bmatrix} = \begin{bmatrix} 1 & -\frac{1}{h} \\ 0 & 1 \end{bmatrix}$$

Unsteady Heat Flow through wall



To simplify again,

When, $s=i\omega$ is used in Laplace transform & using lower limit of integration as $-\infty$; for 1^{st} harmonic.

- All temperature and heat fluxes are multiplied by $e^{-i\omega_1 t}$ & integrated from $-\infty$ to $+\infty$ to obtain the transform

$$\int_0^{\infty} e^{-i\omega_1 t} T(t) dt = \int_{-\infty}^{\infty} T(t) \cos(\omega_1 t) dt - i \int_{-\infty}^{\infty} T(t) \sin(\omega_1 t) dt$$

$$= \pi(a_1 - i b_1)$$

a_1 and b_1 is Fourier's coefficient

Unsteady Heat Transfer



$$\pi(a_1 - ib_1) = \pi T_o e^{-i\omega_1 t}$$

$$T_o = \sqrt{(a_1^2 + b_1^2)}$$

$$\omega_1 = \tan^{-1}(-b_1/a_1)$$

❖ $T(t)$, $q(t)$ thus gets transformed to Fourier amplitude for the corresponding harmonic multiplied by $\pi e^{-i\omega_1 t}$

Transmission Matrix



All temperature & heat fluxes are multiplied by exponent $\pi e^{-i\omega, t}$; $\pi e^{-i\omega, t}$ can be ignored but respective ω , need to be used in the transmission matrix.

$$\begin{bmatrix} T_L \\ q_L \end{bmatrix} = \begin{bmatrix} m_{11} & m_{12} \\ m_{21} & m_{22} \end{bmatrix} \begin{bmatrix} T_o \\ q_o \end{bmatrix}$$

$$m_{11} = m_{22} = \cosh \sqrt{\frac{i\omega}{\alpha}} l;$$

$$m_{12} = - \frac{1}{k \sqrt{\frac{i\omega}{\alpha}}} \sinh \sqrt{\frac{i\omega}{\alpha}} l$$

$$m_{21} = - k \sqrt{\frac{i\omega}{\alpha}} \sinh \sqrt{\frac{i\omega}{\alpha}} l$$

Transmission Matrix



$$i^{1/2} (w/\alpha)^{1/2} = (2i)^{1/2} (w/2\alpha)^{1/2}$$

$$(2i)^{1/2} = [(1+i)^2]^{1/2} = 1+i$$

$$F = (w/2\alpha)^{1/2}$$

$$m_{11} = \cosh (Fl + iFl)$$

$$m_{12} = - \sinh (Fl + iFl) / (kF + ikF)$$

$$m_{21} = (-kF + ikF) \sinh (Fl + iFl)$$

$$m_{22} = \cosh (Fl + iFl)$$

Transmission Matrix



$$\begin{bmatrix} T(l) \\ q(l) \end{bmatrix} = \begin{bmatrix} A & B \\ C & D \end{bmatrix} \begin{bmatrix} T(0) \\ q(0) \end{bmatrix}$$

OR

$$\begin{bmatrix} T_i \\ q_i \end{bmatrix} = \begin{bmatrix} A & B \\ C & D \end{bmatrix} \begin{bmatrix} T_o \\ q_o \end{bmatrix}$$

Admittance factor (\tilde{Y}):

This is defined as the **amount of energy entering a surface for each degree of temperature swing** at the environmental point.

It is used to represent enclosure response to give the equivalent swing in temperature about some mean value due to a cyclic load on an enclosure.

Consequently mathematically defined as,

$$\tilde{Y}(l,t) = \frac{q(l,t)}{T(0,t)} = \frac{q_i}{T_i} = \text{heat flux/swing of inside temperature}$$

q_i will be found by decrement factor and utilised here to find the internal room temperature

Admittance response factor



\tilde{Y} can be determined from transmission matrix, assuming constant outside temperature, i.e. $\check{T}_o=0$

$$\begin{bmatrix} T_i \\ q_i \end{bmatrix} = \begin{bmatrix} A & B \\ C & D \end{bmatrix} \begin{bmatrix} T_o \\ q_o \end{bmatrix}$$

For $\check{T}_o = 0$

$$T_i = Bq_o$$

$$q_i = Dq_o$$

$$\tilde{Y} = \frac{q_i}{T_i} = \frac{D}{B}$$

Frequency Domain response Factor



To simplify again,

Decrement response factor (μ):

This is defined as the ratio of the cyclic flux transmission to the steady state flux transmission. (Or temperature)

It is applied to fluctuations (about mean) in external temperature or flux harmonics impinging on exposed opaque surfaces undergoing transient heat transfer.

Consequently mathematically defined as,

$$\tilde{U} = \frac{q(l,t)}{T(0,t)} = \frac{qi}{T_o} = \text{heat flux/swing of outside temperature}$$

$$\mu = \frac{\tilde{U}}{U}$$

Decrement response factor



μ can be determined from Transmission matrix assuming constant inside temperature i.e. $\check{T}_i = 0$

$$\begin{bmatrix} T_i \\ q_i \end{bmatrix} = \begin{bmatrix} A & B \\ C & D \end{bmatrix} \begin{bmatrix} T_o \\ q_o \end{bmatrix}$$

$$\begin{bmatrix} T_o \\ q_o \end{bmatrix} = \begin{bmatrix} A & B \\ C & D \end{bmatrix}^{-1} \begin{bmatrix} T_i \\ q_i \end{bmatrix}$$

$$\begin{bmatrix} T_o \\ q_o \end{bmatrix} = \begin{bmatrix} D & -B \\ -C & A \end{bmatrix} \begin{bmatrix} T_i \\ q_i \end{bmatrix}$$

$$\text{For } \check{T}_i = 0 \quad T_o = -Bq_i$$

$$\tilde{U} = \frac{q_i}{T_o} = \frac{1}{-B} \quad \mu = \frac{1}{U(-B)}$$

Decrement Factor



$$M' = \text{inv}(M)$$

$$1/-B = 1/M' (1,2);$$

$$U = (1/(1/h_o + l/k + 1/h_i))$$

$$\text{(Complex decrement) } C_{\text{dec}} = 1/-BU$$

$$\mu = \text{abs}(c_{\text{dec}})$$

$$\phi = \text{angle}(c_{\text{dec}}/U) \pi * 12$$

$$1/-BU = X + iY$$

$$\mu = \sqrt{X^2 + Y^2}$$

$$\text{Tan}(\phi) = Y/X$$

Ventilation Heat Exchange (Q_{cv})



Outside air coming In= Inside air going out

If air flow = $V \text{ m}^3/\text{sec}$

i.e. volume exchange in unit time (sec) = $V \text{ m}^3$

C_p – Specific heat of air at constant pressure

P = Density of air

$$Q_{cv} = \rho V C_p (T_{oa} - T_{ia})$$

ρC_p – Volumetric heat capacity = 1300 Joules/K. m^3

V_R = Volume of room

N = Number of air change per hr.

$$Q_{cv} = 1300/3600 N V_R (T_{oa} - T_{ia}) = 1/3 N V_R (T_{oa} - T_{ia})$$

Radiation Heat Exchange (Q_R)



$$Q_R = \sum I A W \theta$$

Where,

I = Intensity of radiation (W/m^2)

θ – Solar Gain factor = 1 for open windows

A_W - Area of Window

Casual Heat Gain (Q_{cs})

$$Q_{cs} = \sum m_i Q_i$$

Mean Temperature in the space



$$\bar{Q}_{cd} = \sum U_j A_j (T_{oe} - T_{ia}) = \sum U_j A_j (T_{oa} + (\alpha l / h_o)_j - T_{ia})$$

Toe- Equivalent sol air temperature

$$\bar{Q}_{cd} = \sum U_j A_j (T_{oa} - T_{ia}) + \sum U_j A_j (\alpha l / h_o)_j$$

For steady state mean temperature

$$\bar{Q}_{cd} + \bar{Q}_R + \bar{Q}_{cv} + \bar{Q}_{cs} = 0$$

If inside & out side mean temperature constant.

Q_R and Q_{cs} - Heat gain

Q_{cd} & Q_{cv} - Heat loss

Mean Temperature in the space



$$\sum U_j A_j (\bar{T}_{oa} - \bar{T}_{ia}) + \sum U_j A_j (\alpha \bar{i} / h_o)_j + \sum A \bar{i} \theta + \bar{C}_V$$

$$(\bar{T}_{oa} - \bar{T}_{ia}) + \bar{Q}_{cs} = 0$$

$$\sum U_j A_j (\bar{T}_{oa} - \bar{T}_{ia}) + \bar{C}_V (\bar{T}_{oa} - \bar{T}_{ia}) + \bar{Q} = 0$$

$$(\bar{T}_{oa} - \bar{T}_{ia}) = -\bar{Q} / (\sum U_j A_j + \bar{C}_V)$$

$$\bar{T}_{ia} = \bar{T}_{oa} + \{\bar{Q} / (\sum U_j A_j + \bar{C}_V)\}$$

Where,

$$\bar{Q} = \sum U_j A_j (\alpha \bar{i} / h_o)_j + \sum A \bar{i} \theta + \bar{Q}_{cs}$$

Mean Temperature in the space



A room 6 m x 5 m x 3m (ht) with one external wall on the long axis has a single glazed window 4.5 m x 2 m facing south. Calculate the mean internal temperature given that $T_{oa} = 17^\circ \text{C}$ and the mean global irradiance on exposed wall is 180 W/m^2 . Assume α of solid wall = 0.4 and $h_o = 9 \text{ W/m}^2$.

$$U_{\text{wall}} = 0.7. U_{\text{window}} = 5.6.$$

Assume two air changes per hour for the room and all adjacent room to be the same temperature. Solar gain factor for glass = 0.76.

Mean Temperature in the space



$$V_R = 6 \times 5 \times 3 = 90 \text{ m}^3$$

$$A_{\text{window}} = 4.5 \times 2 = 9 \text{ m}^2$$

$$A_{\text{wall}} = 6 \times 3 - 9 = 9 \text{ m}^2$$

$$I = 180 \text{ W/m}^2$$

$$\text{Mean heat gain through wall} = UA (\alpha I / h_o)$$

$$= 0.7 \times 9 \times 0.4 \times 180 / 9 = 50.4 \text{ W}$$

$$\text{Mean heat gain through window} = A I \theta$$

$$= 9 \times 180 \times 0.76 = 1231.2 \text{ W}$$

Mean Temperature in the space



$$C_V = \frac{1}{3} N V_R = \frac{1}{3} * 2 * 90 = 60 \text{ W/}^\circ\text{C}$$

$$U_j A_j = 0.7 * 9 + 5.6 * 9 = 56.7$$

$$\bar{T}_{ia} = \bar{T}_{oa} + \{ \bar{Q} / (\sum U_j A_j + \bar{C}_V) \}$$

$$\begin{aligned} T_{ia} &= 17 + \{ 1281.6 / (60 + 56.7) \} \\ &= 17 + \{ 1281 / 116.7 \} \\ &= 27.9^\circ\text{C} \end{aligned}$$

Recall, Mean Room temperature

$$\check{T}_i = \check{T}_o + \frac{\bar{Q}_T}{(\sum AU + Cv)}$$

$$\bar{Q}_T = \bar{Q}_R + \bar{Q}_{cs}$$

Room temperature at any instant t is:

$$T_i(t) = \check{T}_i + \check{T}_i(t) \text{ (Fluctuating component)}$$

$\check{T}_i(t)$ swing needs to be obtained

Fluctuating Heat gains



The total fluctuating energy gain at the environmental point and due to any particular excitation frequency is given by:

$$\tilde{Q}_T(t) = \tilde{Q}_{fs}(t) + \tilde{Q}_S(t) + \tilde{Q}_c(t) + \tilde{Q}_{fc}(t) + \tilde{Q}_v(t)$$

Where,

$\tilde{Q}_{fs}(t)$ - Solar radiation on Opaque body fluctuating heat gain

$\tilde{Q}_S(t)$ - Transparent surface solar fluctuating heat gain

$\tilde{Q}_c(t)$ - Casual gain fluctuating heat

$\tilde{Q}_{fc}(t)$ - Opaque surface fluctuating heat gain

$\tilde{Q}_{gc}(t)$ - Transparent surface conduction fluctuating heat gain

$\tilde{Q}_v(t)$ - Fluctuating ventilation heat transfer

Fluctuating Heat gains



Solar radiation on Opaque body fluctuating heat gain $\tilde{Q}_{fs}(t) =$

$$\tilde{Q}_{fs}(t) = \sum_{i=1}^N [A_i U_i R_o \mu_i \alpha_i \tilde{I}_{so}(t - \phi_d)]$$

Opaque surface fluctuating heat gain $\tilde{Q}_{fc}(t) =$

$$\tilde{Q}_{fc}(t) = \sum_{i=1}^O [A_i U_i \mu_i \tilde{T}_o(t - \phi_d)]$$

Where,

$\mu - \frac{\tilde{U}}{U}$ = Decrement response factor

$R_o = 1/h_o$ = surface heat transfer resistance coefficient

ϕ_d is decrement time lag

$$\tilde{I}_{so}(t - \phi_d) = I_{so}(t - \phi_d) - \bar{I}_{so}$$

Fluctuating Heat gains and Internal temperature



Fluctuating heat gain through surfaces and gain of air is equal to fluctuating heat input over mean

$$\tilde{T}_i(t) \left(\sum AY + C_v \right) = \tilde{Q}_T(t - \phi_a)$$
$$\tilde{T}_i(t) = \frac{\tilde{Q}_T(t - \phi_a)}{(\sum AY + C_v)}$$

Where, Y is admittance factor

ϕ_a = time lag



Thermal Admittance



- Thermal performance of the wall/roofs can be measured by two parameters: **thermal insulation and thermal mass.**
- **Thermal transmittance is a steady-state property and it is the measure of thermal insulation**
- **Thermal admittance (w/mk) is the measure of thermal mass. An ability to absorb the heat from and release it to a space over time.**
- **Amount of energy leaving the internal surface of the element into the room per unit degree of temperature swing**



Thermal Admittance



- This can be used for **thermal storage capacity** of a materials absorbing heat from and releasing it to a space through cyclic temperature variations and thus evening out temperature variations and so reducing the building services system.
- This is a measure of the ability of a surface to smooth out temperature variations in a space and represents the rate of energy entry into a structure rather than that of passage through it.

For reduced cooling loads, thermal transmittance should be as low as possible and thermal admittance should be as high as possible.



Thermal transmittance

- Thermal transmission through unit area of a building unit divided by the temperature difference between the air or other fluid on either side of the building unit in steady state conditions is termed as Thermal Transmittance (*U-value*).

Overall U- factor of typical wall assembly construction:

$$U = 1 / (1/h_i + \sum_{i=1}^n L_i / K_i + 1/ h_o) \dots \dots \dots (i)$$

Where, h_o (19.90 W/(m² K) and h_i (9.3 W/(m² K) are the outside and inside film heat transfer coefficients, L_i and K_i are thicknesses and thermal conductivities of material layers.

- A measure of the **overall ability** of a building element (wall / window / floor / roof) to prevent heat loss (W/m²K).

It includes: Material resistances, surface resistances & air space resistances



Energy Conservation Building Code



ECBC

Energy
Conservation
Building
Code 2017

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The provisions of this code apply to:

(a) Building envelope

(b) Thermal comfort systems and controls (only those installed by developer/ owner)

(c) Lighting systems and controls (only those installed by developer/ owner)

(d) Electrical systems (installed by developer/ owner)

(e) Renewable energy systems



GOVERNMENT OF INDIA
MINISTRY OF POWER



Bureau of Energy Efficiency
Ministry of Power, Government of India





ECBC 2017 Requirements



Table 4.7 Opaque Assembly Maximum U-factor (W/m²) Requirements for a ECBC compliant building

	Composite	Hot and dry	Warm and humid	Temperate	Cold
All building types, except below	0.40	0.40	0.40	0.55	0.34
No Star Hotel < 10,000AGA	0.63	0.63	0.63	0.63	0.40
Business <10,000AGA	0.63	0.63	0.63	0.63	0.40
School <10,000AGA	0.85	0.85	0.85	1.00	0.40

Table 4.8 Opaque Assembly Maximum U-factor (W/m²) Requirements for a ECBC + compliant building

	Composite	Hot and dry	Warm and humid	Temperate	Cold
All building types, except below	0.34	0.34	0.34	0.55	0.22
No Star Hotel < 10,000AGA	0.44	0.44	0.44	0.44	0.34
Business <10,000AGA	0.44	0.44	0.44	0.55	0.34
School <10,000AGA	0.63	0.63	0.63	0.75	0.44

Table 4.7 Opaque Assembly Maximum U-factor (W/m²) Requirements for Super ECBC building

	Composite	Hot and dry	Warm and humid	Temperate	Cold
All building types	0.22	0.22	0.22	0.22	0.22

Energy Conservation Building Code (Code) is to provide minimum requirements for the energy-efficient design and construction of buildings



Roof Assembly Max. *U*-factor Requirements



The Roof Insulation shall be applied externally as part of the Structural Slab and **not as part of the False Ceiling**

Table 4.4 Roof Assembly U-factor (W/m²) Requirements for ECBC Compliant building

	Composite	Hot and dry	Warm and humid	Temperate	Cold
All building types, except below	0.33	0.33	0.33	0.33	0.28
School <10,000AGA	0.47	0.47	0.47	0.47	0.33
Hospitality > 10,000AGA	0.20	0.20	0.20	0.20	0.20

Table 4.5 Roof Assembly U-factor (W/m²) Requirements for ECBC + Compliant building

	Composite	Hot and dry	Warm and humid	Temperate	Cold
Hospitality, Healthcare Assembly	0.20	0.20	0.20	0.20	0.20
Business Educational Shopping Complex	0.26	0.26	0.26	0.26	0.20

Table 4.6 Roof Assembly U-factor (W/m²) Requirements Super ECBC building

	Composite	Hot and dry	Warm and humid	Temperate	Cold
All Building types	0.20	0.20	0.20	0.20	0.20



Thermal Transmittance for Different Roofing Systems



Building Sections / Components	U-value (W/m ² K)
R.C. Plank and joist roofing system 60 mm RC plank + 50 mm mud phuska + 50 mm brick tiles + 15 mm cement plaster	2.71
100 mm thick R.B.C slab + 50 mm mud phuska + 50mm brick tiles + 15 mm cement plaster	2.36
Brick panel roofing system: Panel size 1150 x 530 x 76 mm + R.C.C Joist	2.16
115 mm RCC + 75mm Mud Phuska + 50 mm brick tile	2.01

None of the Roofing Assemblies fulfill the ECBC Criteria



Energy Conservation Building Code



ECO-NIWAS SAMHITA 2018 (Energy Conservation Building Code for Residential Buildings)

PART I: BUILDING ENVELOPE



BUREAU OF ENERGY EFFICIENCY (BEE)
Ministry of Power, Government of India
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Energy Conservation Building Code – Residential 2018



- Code sets minimum performance standards for building envelope to limit heat gains (for cooling dominated climates) and limit heat loss (for heating dominated climates) through it.
- RETV is the **net heat gain rate** (over the cooling period) through the **building envelope of dwelling units** (excluding roof) divided by the area of the building envelope (excluding roof) of dwelling units. Its unit is W/m^2

$$RETV = \frac{1}{A_{envelope}} \times \left[\begin{aligned} & \left\{ a \times \sum_{i=1}^n \left(A_{opaque_i} \times U_{opaque_i} \times \omega_i \right) \right\} \\ & + \left\{ b \times \sum_{i=1}^n \left(A_{non-opaque_i} \times U_{non-opaque_i} \times \omega_i \right) \right\} \\ & + \left\{ c \times \sum_{i=1}^n \left(A_{non-opaque_i} \times SHGC_{eq_i} \times \omega_i \right) \right\} \end{aligned} \right]$$

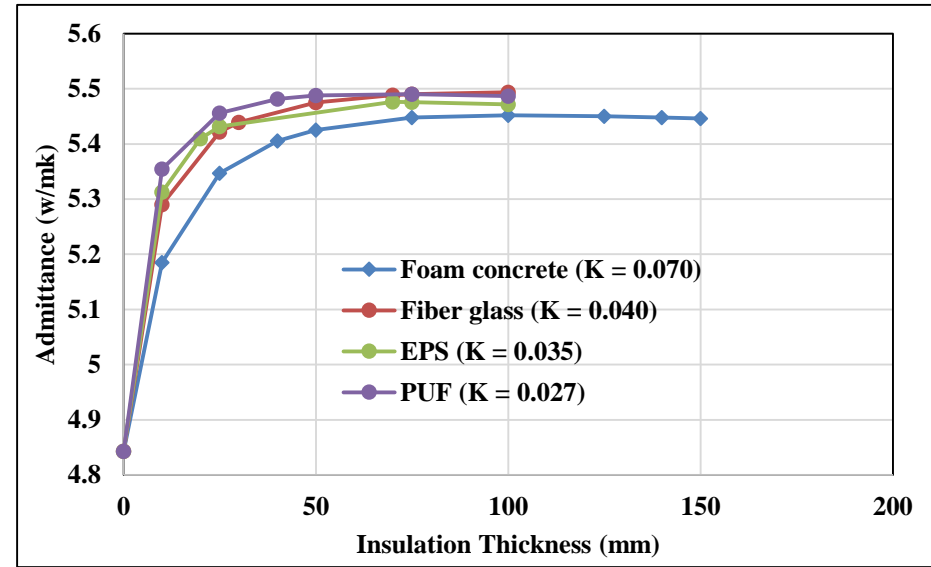
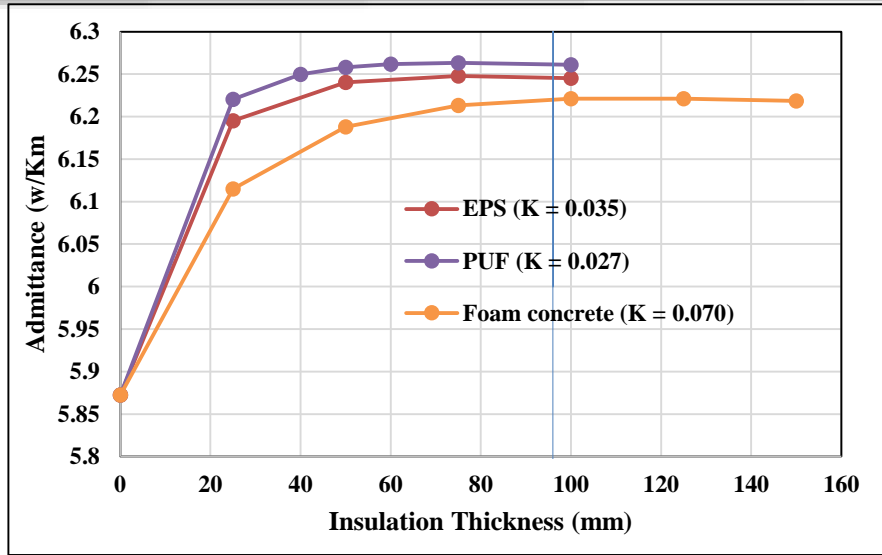
Residential Envelope Transmittance Value (RETV) for building envelope (except roof) shall comply with the maximum RETV of $15 W/m^2$

- Thermal transmittance of the building envelope (except roof) for cold climate shall comply with the maximum of $1.8 W/m^2.K$.**
- Thermal transmittance of roof shall comply with the maximum U_{Roof} value of $1.2 W/m^2K$**



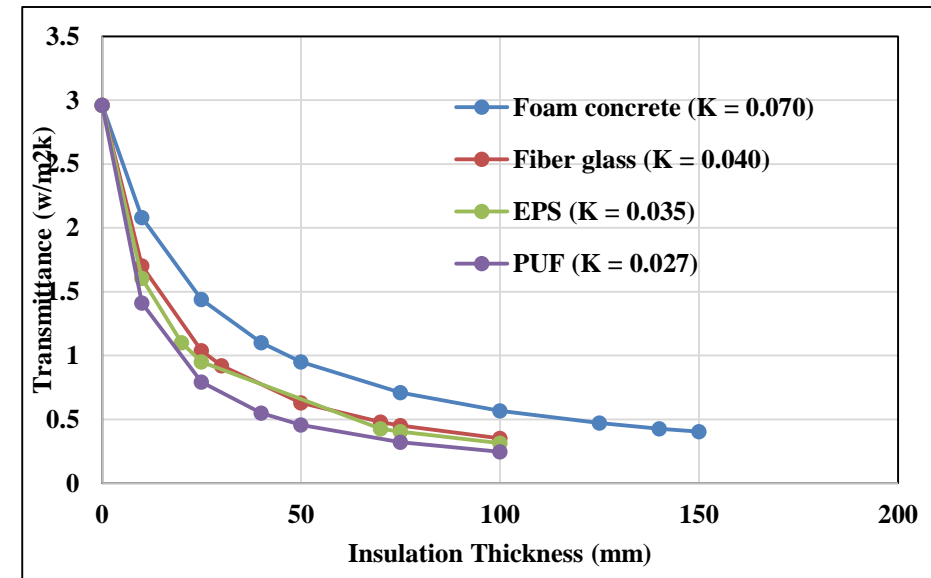
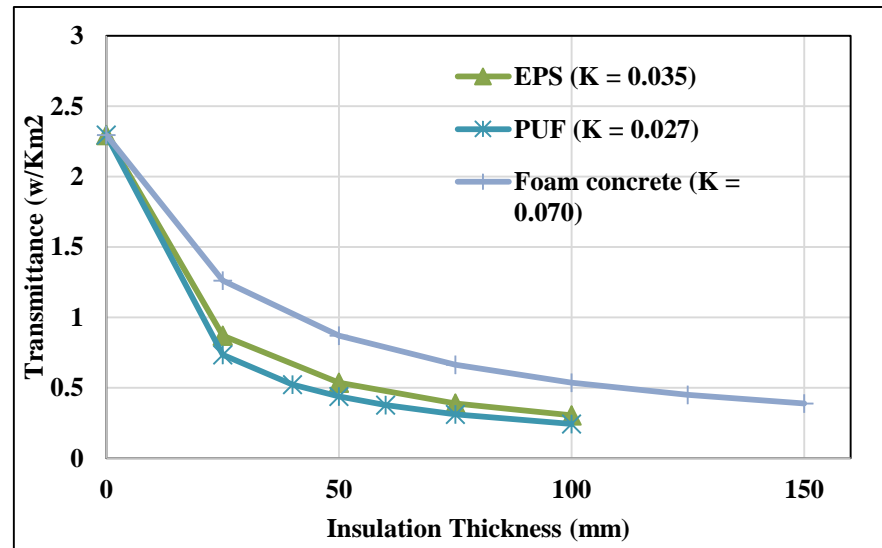
Table 3 Coefficients (a, b and c) for RETV formula

Climate zone	a	b	c
Composite	6.06	1.85	68.99
Hot-Dry	6.06	1.85	68.99
Warm-Humid	5.15	1.31	65.21
Temperate	3.38	3.37	63.69
Cold	Not applicable (Refer Section 3.5)		



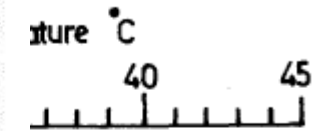
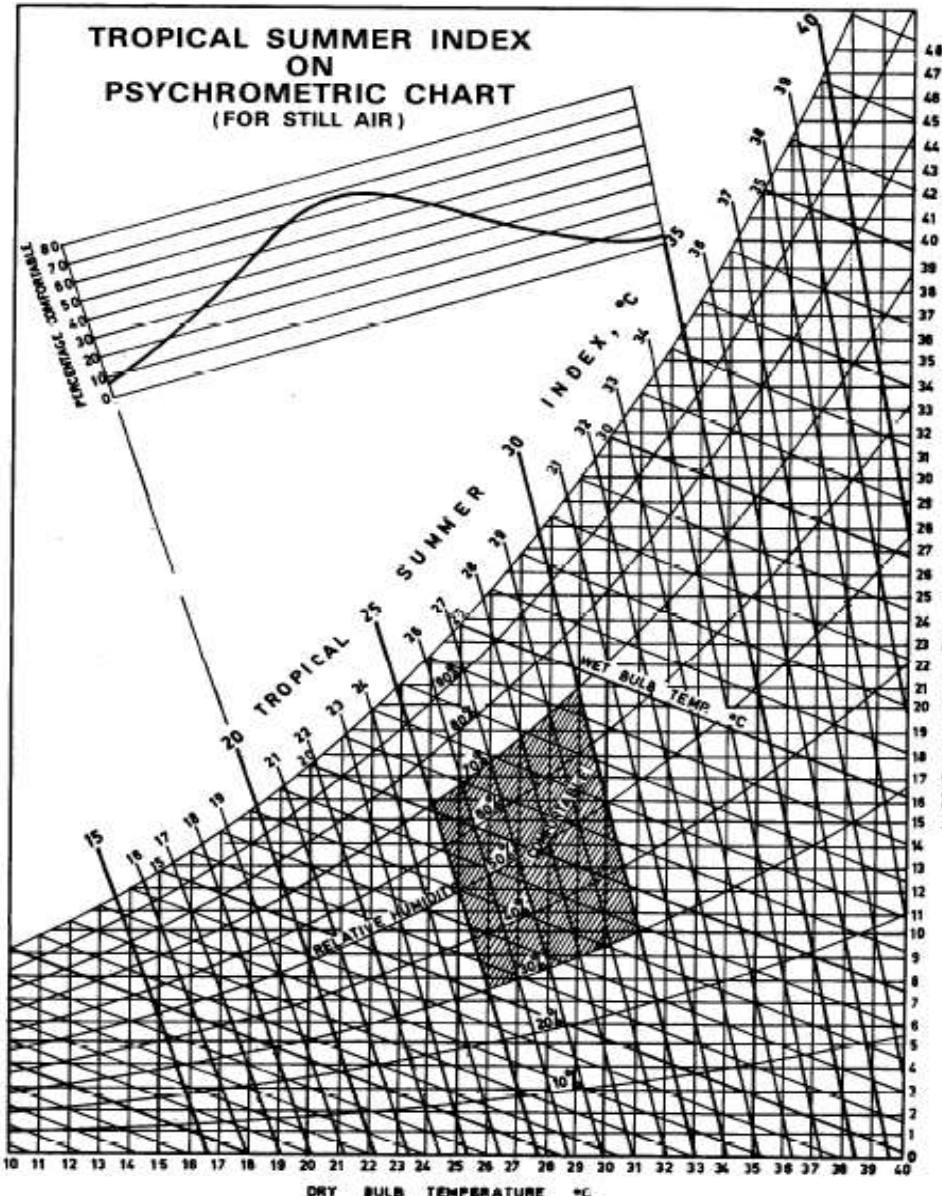
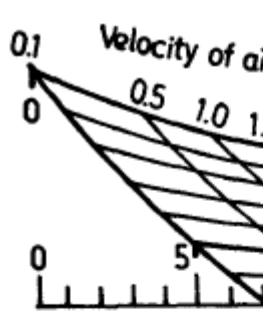
Roof

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CLIMATOLOGY : Thermal Comfort

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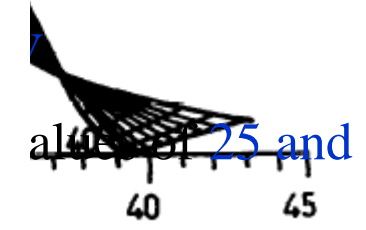
Tropical Summer

- **Definition :** The relative humidity environment.

$$TSI = .308 t_w -$$

- The thermal co 30°C with optimum
- 30-34°C : tolerabl

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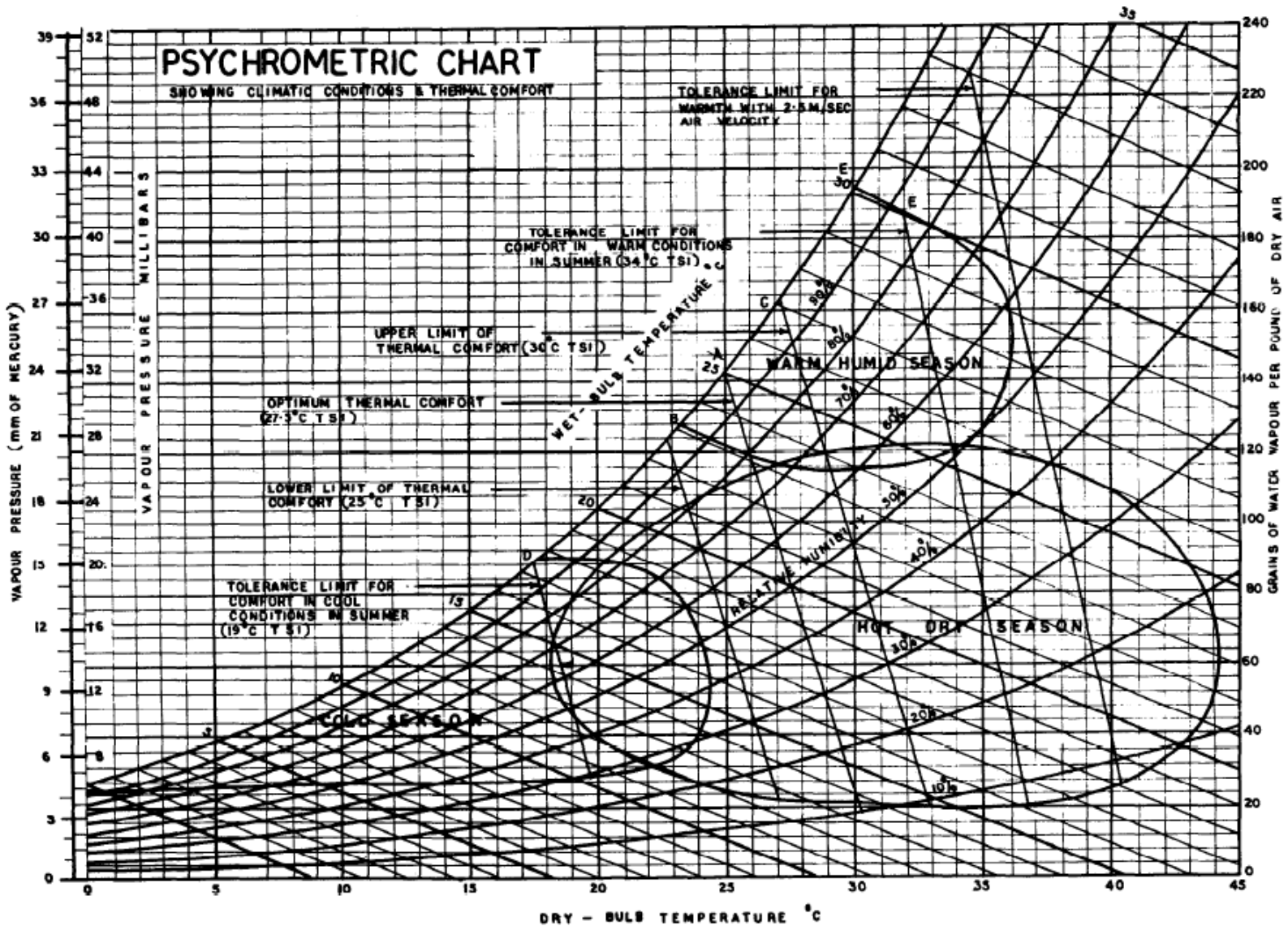


FIG. 3 PSYCHROMETRIC CHART (SHOWING CLIMATIC CONDITIONS AND THERMAL COMFORT)

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Thank You